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(54) Title: AQUEOUS DISPERSIONS OF COMB COPOLYMERS AND COATINGS PRODUCED THEREFROM

(57) Abstract: An aqueous coating composition comprising a comb copolymer is disclosed. A method of forming a coating from the aqueous coating composition, and a coating formed by that method are also disclosed, as is a method of forming the comb copolymer. The comb copolymer is characterized in that aqueous dispersions of the comb copolymer have a Hard/Soft Balance Advantage value of at least 25 %. The aqueous coating composition is capable of producing coatings having an excellent balance of hard and soft properties.

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AQUEOUS DISPERSIONS OF COMB COPOLYMERS AND COATINGS PRODUCED  
THEREFROM

5           This application is a continuation-in-part of Serial No. 60/232,414, filed September 14, 2000.

          The present invention relates to an aqueous dispersion of a comb copolymer, wherein films formed from the aqueous dispersion display an improved balance of properties related to hardness and softness, and to the comb copolymer of which the aqueous dispersion is  
10       comprised.

          Polymeric coatings are typically formed by deposition of a solution or dispersion of a polymer in a solvent or dispersing medium, respectively. Evaporation of the layer thus formed will result in a continuous film for some polymer compositions, but not for others. For example, a dispersion including polymeric particles, the polymeric chains of which have a  
15       glass transition temperature in the range of -90°C to 70°C, may form a continuous film, with the likelihood of such formation increasing for polymers having Tg values near, or below, the temperature at which film formation is attempted, often room temperature. Unfortunately, coatings that are easily formed often exhibit poor hardness related properties. They tend to be “soft” and tacky. This tackiness translates into a tendency for the surface of the film to retain  
20       dirt particles that contact it. Tackiness also translates into “block”, the tendency for two films to stick to one another, or for a single film to stick to itself. The softness further translates into unrecoverable deformation, called “print”. “Print” is observed when an object is placed upon a film and, upon removal, the imprint of the object does not go away.

          It is, therefore, highly desirable to form coatings that have a “hardness” component.  
25       This hardness translates into coatings having surfaces that resist scratching, dirt pick-up, and block. Truly “hard” coatings are difficult to achieve because the relatively high glass transition temperature, “Tg”, required to produce such coatings renders the actual formation of coatings difficult or impossible. When these “hard” coatings are achieved, for example, by adding high levels of a coalescent to an aqueous dispersion of a hard polymer, these coatings  
30       often are so dominated by the hardness characteristic that they fail to exhibit softness characteristics that can contribute to overall performance. Hard coatings are often brittle, lacking the flexibility to elongate and bend, a common requirement during use.

"Coatings" herein include compositions applied to various substrates and commonly identified as architectural coatings such as, for example, flat coatings, semigloss coatings, gloss coatings, clear coatings, primers, topcoats, stain-blocking coatings, penetrating sealers for porous substrates such as chalky surfaces, concrete, and marble, elastomeric coatings, mastics, caulks, and sealants; industrial coatings such as, for example, board and paneling coatings, transportation coatings, furniture coatings, and coil coatings; maintenance coatings such as, for example, bridge and tank coatings and road marking paints; leather coatings and treatments; paper coatings; woven and nonwoven fabric coatings and pigment printing pastes; adhesive coatings such as, for example, pressure sensitive adhesives and wet- and dry-laminating adhesives; automotive coatings; and ink coatings selectively applied to produce printed images, such as letters and pictures, through techniques such as, for example ink-jetting. Coatings having improvement in at least one property such as, for example, block resistance, print resistance, mar resistance, scrub resistance, burnish resistance, dirt pickup resistance, adhesion, gloss, flexibility, toughness, impact resistance, drying time, coalescent demand, water resistance, chemical resistance, and stain resistance have long been sought. Many of these properties are improved by either increasing "hardness" or "softness", so that coatings exhibiting an excellent balance of hardness and softness characteristics have, in particular, been sought.

The invention of US-A-6,060,532 sought, for example, to provide coatings having a good balance of low temperature flexibility, tensile strength, and dirt pick up resistance. Low temperature flexibility is a "softness" characteristic, while tensile strength and dirt pick up resistance are characteristic of "hardness". Coatings were formed from a binder polymer which was an elastomeric multi-stage emulsion polymer obtained by sequentially polymerizing, under emulsion polymerization conditions, a first monomer system free from polyethylenically unsaturated monomers, and which yields a first-stage polymer having a glass transition temperature from about -30°C to about -60°C, and a second monomer system, likewise free from polyethylenically unsaturated monomers, and which yields a second-stage polymer, incompatible with the first-stage polymer, and having a glass transition temperature from 0°C to 60°C. Used herein, these two-stage polymers are referred to a "soft/hard elastomers", or "SHE" polymers. While the SHE polymers of US-A-6,060,532 did improve the balance of hard and soft properties over that of single stage polymers having similar overall compositions, there remained a need for yet further improvement in the hard/soft

balance. It was further desired to achieve that improvement while maintaining excellent film formation behavior for aqueous binder systems completely free of coalescing agents, or containing only low levels of them.

We have, surprisingly, produced comb copolymers and aqueous dispersions of comb  
5 copolymers by a commercially viable method and formed them into coatings having an outstanding balance of properties related to hardness and softness. The polymers can, for example, be utilized in coatings, containing little or no coalescent, cast onto substrate surfaces.

A first aspect of the present invention relates to an aqueous coating composition  
10 comprising a plurality of comb copolymer particles:

wherein said comb copolymer particles comprise a comb copolymer;

wherein said comb copolymer comprises a backbone and at least one graft segment  
attached thereto; and

wherein said comb copolymer is characterized in that an aqueous dispersion comprising  
15 said comb copolymer has a Hard/Soft Balance Advantage value of at least 25%.

A second aspect of the present invention relates to a method of forming a dry coating comprising the steps of:

(a) forming an aqueous coating composition comprising a plurality of comb  
copolymer particles:

20 wherein said comb copolymer particles comprise a comb copolymer;

wherein said comb copolymer comprises a backbone and at least one graft  
segment attached thereto; and

wherein said comb copolymer is characterized in that an aqueous dispersion  
comprising said comb copolymer has a Hard/Soft Balance Advantage value  
25 of at least 25%.

(b) applying said coating composition to a substrate; and

(c) drying, or allowing to dry, said applied coating composition.

A third aspect of the present invention relates to a dry coating comprising a comb  
copolymer:

30 wherein said comb copolymer comprises a backbone and at least one graft segment  
attached thereto; and

wherein said comb copolymer is characterized in that an aqueous dispersion comprising said comb copolymer has a Hard/Soft Balance Advantage value of at least 25%.

A fourth aspect of the present invention relates to a dry coating produced by the method of the second aspect.

5 A further aspect relates to an aqueous coating composition comprising a plurality of comb copolymer particles, wherein the comb copolymer particles comprise comb copolymer, and wherein the comb copolymer is produced by a polymerization method comprising the steps of:

10 (a) forming a macromonomer aqueous emulsion comprising a plurality of water-insoluble particles of macromonomer, wherein said macromonomer comprises polymerized units of at least one first ethylenically unsaturated monomer, said macromonomer further having:

(i) a degree of polymerization of from 10 to 1000;

(ii) at least one terminal ethylenically unsaturated group;

15 (iii) less than 5 weight percent polymerized acid-containing monomer, based on the weight of said macromonomer; and

(iv) less than one mole percent of polymerized mercaptan-olefin compounds;

(b) forming a monomer composition comprising at least one second ethylenically unsaturated monomer; and

20 (c) combining at least a portion of said macromonomer aqueous emulsion and at least a portion of said monomer composition to form a polymerization reaction mixture; and

25 (d) polymerizing said macromonomer with said second ethylenically unsaturated monomer in the presence of an initiator to produce said plurality of comb copolymer particles.

In a still further aspect, the comb copolymer has a weight average molecular weight of 50,000 to 2,000,000.

30 In yet another aspect, the graft segment of the comb copolymer is derived, as a polymerized unit, from a macromonomer; wherein the graft segment comprises, as polymerized units, from 5 weight percent to 50 weight percent of a non-methacrylate monomer, based on the weight of the macromonomer.

In another aspect, the graft segment of the comb copolymer is derived, as a polymerized unit, from a macromonomer; wherein the graft segment comprises, as polymerized units, less than 5 weight percent acid containing monomer, based on the total weight of said macromonomer.

5 In another aspect, the graft segment of the comb copolymer is derived, as a polymerized unit, from a macromonomer, wherein said graft segment has a degree of polymerization of from 10 to 1,000, where the degree of polymerization of said graft segment is expressed as the degree of polymerization of said macromonomer.

10 In another aspect, the graft segment of the comb copolymer has a glass transition temperature of 30°C to 130°C.

In another aspect, the backbone of the comb copolymer has a glass transition temperature of -90°C to 50°C.

Used herein, the following terms have these definitions:

15 The "backbone" of a polymer chain is a collection of polymerized monomer units attached to one another. The attachment is typically achieved by covalent bonding. "Non-terminal" monomer units are directly attached to at least two other monomer units. A "terminal" monomer unit resides at the end of the polymer chain and is directly attached to one other monomer unit. For example, the polymerized monomer units of the backbone may be derived from ethylenically unsaturated monomers.

20 A "linear" polymer (homopolymer or copolymer) is a polymer having a backbone that is not branched. As used herein, the term "linear" is also meant to include polymers wherein a minor amount of branching has occurred. For example, hydrogen abstraction may lead to branching during free radical polymerizations.

25 A "branched" polymer is a polymer having a first "backbone segment" that has other backbone segments (i.e., "branches") chemically attached to it through a "non-terminal" atom of the first backbone segment. Typically, this first backbone segment and all of the branches have the same, or similar, composition. Herein, the term "branching" is used to describe the structure of the backbone of the comb copolymer.

30 A "pendant" group is a group that is attached to the backbone of a polymer. The term pendant may be used to describe a group that is actually part of a polymerized monomer unit. For example, the hydroxyethyl group of a polymerized unit of 2-hydroxyethyl methacrylate may be referred to as a "pendant hydroxyethyl group", or as "pendant hydroxy functionality".

It is also common to refer to large groups attached to a polymer backbone as "pendant" when those large groups are compositionally distinct from the backbone polymer. These large groups may themselves be polymer chains. For example, when a macromonomer becomes incorporated into a polymer chain by reaction with other monomers, the two carbons of its reactive double bond become part of the backbone, while the polymeric chain originally attached to the double bond of the macromonomer becomes a "pendant group" that may, for typically, have a molecular weight of 500 to 100,000. A "pendant" group may further be described as "pendant to" the backbone.

A "terminal" group resides at the end of the polymer chain and is chemically attached to a terminal monomer unit. A terminal group may, for example, have a composition distinct from the composition of the backbone of the polymer. A "pendant" group may occur in a "terminal" position. As such, a "terminal" group is a special case of a "pendant" group.

A "macromonomer" of the present invention is any low molecular weight water-insoluble polymer or copolymer having at least one terminal ethylenically unsaturated group that is capable of being polymerized in a free radical polymerization process. The macromonomer of the present invention preferably has "low water solubility". By "low water solubility" it is meant having a water solubility of no greater than 150 millimoles/liter at 25°C to 50°C. In contrast, the "acid containing macromonomer", described herein below, of the present invention is water soluble. By "low molecular weight" it is meant that the macromonomer has a degree of polymerization of from 5 to 1,000, preferably from 10 to 1,000, more preferably 10 to 200, and most preferably from about 20 to less than 50. By "degree of polymerization" it is meant the number of polymerized monomer units present in the macromonomer. See e.g., Kawakami in the "Encyclopedia of Polymer Science and Engineering", Vol. 9, pp. 195-204, John Wiley & Sons, New York, 1987. Typically, the macromonomer polymer chain contains first ethylenically unsaturated monomers, as polymerized units. Preferably, the first ethylenically unsaturated monomer is selected to impart low water solubility to the macromonomer. Although it is most preferred that every unit of macromonomer have at least one terminal ethylenically unsaturated group that is capable of being polymerized in a free radical polymerization process, the percentage of macromonomer units having such a terminal ethylenically unsaturated group is typically sufficient to prepare the desired comb copolymer of the present invention when that

percentage is less than 70%, preferably at less than 80%, and more preferably at less than 85%.

The term "macromonomer aqueous emulsion" is used herein to describe an aqueous emulsion containing macromonomer dispersed therein as water insoluble particles.

5 A "graft segment" is a polymer chain occupying a pendant position along the polymer backbone. A graft segment may include, as polymerized units, one type of monomer or more than one type of monomer. The composition of a graft segment is different from the composition of the backbone polymer to which it is attached, in contrast to a "branch segment" of a branched backbone which has a composition which is the same as, or similar  
10 to, other portions the branched backbone of which it is a part. A "terminal graft segment" resides at an end of a backbone polymer chain and is chemically attached to that backbone polymer chain. A "terminal graft segment" is a special case of a "pendant graft segment".

"Graft copolymers" are macromolecules formed when polymer or copolymer chains are chemically attached as side chains to a polymeric backbone. Those side chains are the  
15 "graft segments" described herein above. Because graft copolymers often chemically combine unlike polymeric segments in one macromolecule, these copolymers have unique properties compared to the corresponding random copolymer analogues. These properties include, for example, mechanical film properties resulting from thermodynamically driven microphase separation of the copolymer, and decreased melt viscosities resulting in part from  
20 the comb structure of the graft copolymer, and from separation of a soft (i.e., low T<sub>g</sub>) phase. With respect to the latter, reduced melt viscosities can advantageously improve processability of the polymer. *See e.g.*, Hong-Quan Xie and Shi-Biao Zhou, J. Macromol. Sci.-Chem., A27(4), 491-507 (1990); Sebastian Roos, Axel H.E. Müller, Marita Kaufmann, Werner Siol and Clenens Auschra, "Applications of Anionic Polymerization Research", R.P. Quirk, Ed.,  
25 ACS Symp. Ser. 696, 208 (1998).

The term "comb copolymer," as used herein, is a type of graft copolymer, wherein the polymeric backbone of the graft copolymer is linear, or essentially linear, and, preferably, each side chain (graft segment) of the graft copolymer is formed by a "macromonomer" that is grafted to the polymer backbone. The comb copolymers may, for example, be prepared by  
30 the free radical copolymerization of macromonomer with conventional monomer (e.g., second ethylenically unsaturated monomer). The "graft copolymer" of the present invention is a "comb copolymer", and the terms "graft copolymer" and "comb copolymer" are used



interchangeably herein. Used herein a comb copolymer may be one, or more than one type of comb copolymer, i.e., at least one comb copolymer.

A "random copolymer" is a copolymer having monomers, as polymerized units, randomly distributed along its backbone. Used herein, the term "random" has its usual  
5 meaning in the art of polymerization. For example, the distribution of monomer units along a polymer chain prepared by emulsion polymerization is dictated not only by the relative amounts of each type of monomer present at any point during the polymerization, but also by such factors as, for example, the tendency of each monomer type to react with itself relative to its tendency to react with each of the other types of monomer present. These reactive  
10 tendencies are defined by reactivity ratios which are well known for many monomer combinations. See e.g., G. Odian "Principles of Polymerization", Third Edn., pp. 460-492, John Wiley & Sons, New York, 1991.

The term "SHE copolymer" refers to a "soft/hard elastomer" which is a multi-stage copolymer prepared by sequentially polymerizing, under emulsion polymerization conditions,  
15 first monoethylenically unsaturated monomers to yield a first-stage polymer having a Tg of -30°C to -60°C, and then polymerizing second monoethylenically unsaturated monomers to yield a second-stage polymer having a Tg of 0°C to 60°C. The SHE copolymer further includes low levels (up to 5 percent by weight, based on total copolymer) of either a photosensitive benzophenone or phenylketone compound, or a photosensitive benzophenone  
20 monomer, as polymerized units. The SHE copolymers referred to herein are disclosed in US-A-6,060,532.

An "oligomer" is a polymer having a low molecular weight. By "low molecular weight" it is meant that the oligomer has a degree of polymerization of from 5 to 1,000, preferably from 10 to 1,000, more preferably 10 to 200, and most preferably from about 20 to  
25 less than 50.

An "aqueous dispersion of a comb copolymer" is an aqueous medium in which are dispersed a plurality of particles of comb copolymer. Used herein, an "aqueous dispersion of a comb copolymer" is an "aqueous copolymer composition".

"Tg" is the "glass transition temperature" of a polymeric phase. The glass transition  
30 temperature of a polymer is the temperature at which a polymer transitions from a rigid, glassy state at temperatures below Tg to a fluid or rubbery state at temperatures above Tg. The Tg of a polymer is typically measured by differential scanning calorimetry (DSC) using

the mid-point in the heat flow versus temperature transition as the Tg value. A typical heating rate for the DSC measurement is 20 Centigrade degrees per minute. The Tg of various homopolymers may be found, for example, in *Polymer Handbook*, edited by J. Brandrup and E. H. Immergut, Interscience Publishers. The Tg of a copolymer is estimated by using the Fox equation (T.G. Fox, *Bull. Am. Physics Soc.*, Volume 1, Issue No. 3, page 123 (1956)). A two-phase system resulting from the formation of a coating from a comb copolymer having two types of segment, each immiscible with the other, typically yields two measurable glass transition temperatures. For such a comb copolymer, one Tg can be measured, or calculated, for the phase formed by the backbone, and another Tg for the phase formed by the graft segment. An "average Tg", or "overall Tg" may be calculated for such systems as a weighted average of the amount of polymer in each phase of a given Tg. This average Tg for a two-phase system will equal the single Tg calculated for a random copolymer having the same overall composition as that of a copolymer for which two Tg values may be calculated or measured.

"Effective Tg". When a substance having some degree of solubility in a polymer is imbibed by that polymer, the softening temperature of the polymer decreases. This plasticization of the polymer can be characterized by measuring the "effective Tg" of the polymer, which typically bears an inverse relationship to the amount of solvent or other substance contained in the polymer. The "effective Tg" of a polymer containing a known amount of a substance dissolved within is measured just as described above for "Tg". Alternatively, the "effective Tg" may be estimated by using the Fox equation (*supra*), assuming a value for Tg (e.g., the freezing point) of the solvent or other substance contained in the polymer.

Molecular Weight. Synthetic polymers are almost always a mixture of chains varying in molecular weight, i.e., there is a "molecular weight distribution", abbreviated "MWD". For a homopolymer, members of the distribution differ in the number of monomer units which they contain. This way of describing a distribution of polymer chains also extends to copolymers. Given that there is a distribution of molecular weights, the most complete characterization of the molecular weight of a given sample is the determination of the entire molecular weight distribution. This characterization is obtained by separating the members of the distribution and then quantitating the amount of each that is present. Once this

distribution is in hand, there are several summary statistics, or moments, which can be generated from it to characterize the molecular weight of the polymer.

The two most common moments of the distribution are the “weight average molecular weight”, “ $M_w$ ”, and the “number average molecular weight”, “ $M_n$ ”. These are defined as follows:

$$M_w = \frac{\sum(W_i M_i)}{\sum W_i} = \frac{\sum(N_i M_i^2)}{\sum N_i M_i}$$

$$M_n = \frac{\sum W_i}{\sum (W_i / M_i)} = \frac{\sum (N_i M_i)}{\sum N_i}$$

where:

$M_i$  = molar mass of  $i^{\text{th}}$  component of distribution

$W_i$  = weight of  $i^{\text{th}}$  component of distribution

$N_i$  = number of chains of  $i^{\text{th}}$  component

and the summations are over all the components in the distribution.  $M_w$  and  $M_n$  are typically computed from the MWD as measured by Gel Permeation Chromatography (see the Experimental Section).

“Particle size” is the diameter of a particle.

The “average particle size” determined for a collection of particles (e.g., macromonomer particles, or particles of graft copolymer) the “weight average particle size”, “ $d_w$ ”, as measured by Capillary Hydrodynamic Fractionation technique using a Matec CHDF 2000 particle size analyzer equipped with a HPLC type Ultra-violet detector.

The “Advantage term”, designated “A” herein, is a term that defines the performance of an aqueous dispersion of a comb copolymer in a specific test, or a battery of tests, relative to a control, which is an aqueous dispersion of a random copolymer having the same overall composition as the comb copolymer with which it is being compared. The advantage term for performance in a single test is defined as follows:

$$A = [(P/P_{\text{control}}) - 1] \times 100\%,$$

where P is the performance of a first material, as an aqueous dispersion, in a given test, and  $P_{\text{control}}$  is the performance in the same test of another material, as an aqueous dispersion, with which that first material is being compared. The value of an "Advantage term" is referred to as the corresponding "Advantage value", given in units of percent. In determining the value of the Advantage term (i.e., the "Advantage value") for an aqueous dispersion of a given comb copolymer, the control aqueous dispersion is that of a random copolymer having the same overall composition as the comb copolymer being compared to it, and present in the aqueous dispersion at the same concentration as the comb copolymer. When the "Advantage value" for an aqueous dispersion of a polymer-polymer or polymer-oligomer blend is determined herein, the control polymer is an aqueous dispersion of a random copolymer having the same overall composition as the blend. For example, a 50:50 (weight:weight) blend of polymer A composed of, as polymerized units, 30 mole percent of monomer X and 70 mole % of monomer Y, with polymer B composed of, as polymerized units, only monomer Y, would be compared with a random copolymer having 15 mole % of monomer X and 85 mole % of monomer Y.

Four tests measuring "hardness" are described herein and utilized to differentiate among various copolymers (as aqueous dispersions) in the Experimental Section herein below. " $A_K$ ", " $A_T$ ", " $A_S$ ", and " $A_B$ " are the advantage terms derivable from the "Konig Pendulum Hardness", "Finger Tack", "Tensile Strength", and "Peel Block Resistance" tests, respectively. As such, they are referred to as the "Konig Hardness Advantage term", the "Tack Advantage term", the "Tensile Strength Advantage term", and the "Block Advantage term", respectively. Used herein, "Konig" and "Konig Hardness" may be used interchangeably with "Konig Pendulum Hardness"; "Tack" may be used interchangeably with "Finger Tack", and "Block" and "Block Resistance" may be used interchangeably with "Peel Block Resistance".

Two tests measuring "softness" are described herein and utilized to differentiate among various copolymers (as aqueous dispersions) in the Experimental Section herein below. " $A_E$ ", and " $A_F$ " are the advantage terms derivable from the tensile elongation test and the low temperature mandrel flexibility test, respectively. As such, they are referred to as the "Elongation Advantage term" and the "Flexibility Advantage term", respectively. The temperature selected for the mandrel flexibility test is chosen to be equal to or less than the

overall glass transition temperature,  $T_g$ , of the copolymer film being tested. This temperature is chosen, herein, to be  $-35^{\circ}\text{C}$ , unless specified otherwise.

For any given material, the average of the experimentally determined values for the four "hardness" advantage terms are averaged to give the "Hardness Advantage Term", " $A_{\text{Hard}}$ ". Similarly, the average of the experimentally determined values for the two "softness" advantage terms are averaged to give the "Softness Advantage Term", " $A_{\text{Soft}}$ ". " $A_{\text{Hard}}$ " and " $A_{\text{Soft}}$ " are then averaged to give " $A_{\text{HSB}}$ ", the "Hard/Soft Balance Advantage term", abbreviated herein as " $A_{\text{HSB}}$ ". The following expressions define " $A_{\text{Hard}}$ ", " $A_{\text{Soft}}$ ", and " $A_{\text{HSB}}$ ":

$$A_{\text{Hard}} = (A_K + A_T + A_S + A_B) / 4;$$

$$A_{\text{Soft}} = (A_E + A_F) / 2; \text{ and}$$

$$A_{\text{HSB}} = (A_{\text{Hard}} + A_{\text{Soft}}) / 2.$$

In any equation for an Advantage term used herein to describe performance in a given test, it is assumed that "P" and " $P_{\text{control}}$ " (see the general equation for "A" above) are measured by that test method, so that there is no need to provide additional subscripts for those performance terms.

When a material does not form a film under the conditions of film formation used in preparing specimens for the tests, each advantage term is assigned a value of -100%. In such cases, " $A_{\text{HSB}}$ " also becomes -100%. " $A_{\text{HSB}}$ " is then a good measure of the three-way balance of film hardness, film softness, and the ability to form a film.

The comb copolymer of the present invention is characterized in that aqueous dispersions produced therefrom preferably have Hard/Soft Balance Advantage Values of at least 25%, more preferably from 40% to 1,500%, and most preferably from 100% to 1,000%.

Estimation of whether a polymer and another component (i.e., another polymer or a solvent) will be miscible may be made according to the well-known methods delineated in D. W. Van Krevelen, *Properties of Polymers*, 3<sup>rd</sup> Edition, Elsevier, pp. 189-225, 1990. For example, Van Krevelen defines the total solubility parameter ( $\delta_t$ ) for a substance by:

$$\delta_t^2 = \delta_d^2 + \delta_p^2 + \delta_h^2,$$

where  $\delta_d$ ,  $\delta_p$ , and  $\delta_h$  are the dispersive, polar, and hydrogen bonding components of the solubility parameter, respectively. Values for  $\delta_d$ ,  $\delta_p$ , and  $\delta_h$  have been determined for

many solvents, polymers, and polymer segments, and can be estimated using the group contribution methods of Van Krevelen. For example, to estimate whether a polymer having a given composition will be miscible with a particular solvent, one calculates  $\delta_t^2$  for the polymer and  $\delta_s^2$  for the solvent. Typically, if the difference between the two,  $\Delta\delta_t^2$ , is greater than 25 (i.e.,  $\Delta\delta_t > 5$ ), then the polymer and the solvent will not be miscible.

If, instead, it is desired to determine whether two polymers, differing in composition, will be miscible, the same calculations may be carried out, but the predicted upper limit of  $\Delta\delta_t^2$  for miscibility will decrease as the molecular weight of one or both of polymers under consideration increases. This decrease is thought to parallel the decrease in entropy of mixing which occurs as the molecular weight of the components being mixed increases. For example, two polymers, each having a degree of polymerization of 100, will likely be immiscible even if the value of  $\Delta\delta_t^2$  for their mixture is 9, or even 4 (i.e.,  $\Delta\delta_t = 3$ , or even 2). Still higher molecular weight polymers may be immiscible at even lower values of  $\Delta\delta_t$ . To estimate whether a graft segment of the comb copolymer of the present invention, having a given composition, will be miscible with a backbone having another composition, one calculates  $\delta_t^2$  for the graft segment and  $\delta_b^2$  for the backbone. Typically, if the difference between the two,  $\Delta\delta_t^2$ , is greater than 9 (i.e.,  $\Delta\delta_t > 3$ ), then the graft segment should be immiscible with the backbone such that a film formed by the comb copolymer would have two distinct types of polymeric phase. It should be noted, however, that immiscibility between two polymers having degrees of polymerization of approximately 100 or more may occur even when the calculated value of  $\Delta\delta_t^2$  is between 1 and 9 (i.e.,  $\Delta\delta_t$  of 1 to 3), due to the unfavorable entropy effects associated with very long polymeric chains. Similar calculation can be performed to determine whether a film formed from a block copolymer will have more than one polymeric phase. Because it is desirable that the graft segment not be miscible with the backbone, the Van Krevelen calculations of miscibility provide useful estimates of whether a given pair of compositions of the graft segment and backbone will result in phase separation in, for example, films formed from the comb copolymer.

The macromonomer of the present invention is present in the macromonomer aqueous emulsion as water insoluble particles. The macromonomer is any low molecular weight water-insoluble polymer or copolymer having at least one terminal ethylenically unsaturated group that is capable of being polymerized in a free radical polymerization process.

The macromonomer contains, as polymerized units, at least one first ethylenically unsaturated monomer. Preferably, the first ethylenically unsaturated monomer is selected to impart low or no water solubility to the macromonomer as previously described herein.

Suitable first ethylenically unsaturated monomers for use in preparing macromonomer include for example methacrylate esters, such as C<sub>1</sub> to C<sub>18</sub> normal or branched alkyl esters of methacrylic acid, including methyl methacrylate, ethyl methacrylate, n-butyl methacrylate, lauryl methacrylate, stearyl methacrylate; acrylate esters, such as C<sub>1</sub> to C<sub>18</sub> normal or branched alkyl esters of acrylic acid, including methyl acrylate, ethyl acrylate, n-butyl acrylate and 2-ethylhexyl acrylate; styrene; substituted styrenes, such as methyl styrene, a-methyl styrene or t-butyl styrene; olefinically unsaturated nitriles, such as acrylonitrile or methacrylonitrile; olefinically unsaturated halides, such as vinyl chloride, vinylidene chloride or vinyl fluoride; vinyl esters of organic acids, such as vinyl acetate; N-vinyl compounds such as N-vinyl pyrrolidone; acrylamide; methacrylamide; substituted acrylamides; substituted methacrylamides; hydroxyalkylmethacrylates such as hydroxyethylmethacrylate; hydroxyalkylacrylates; basic substituted (meth)acrylates and (meth)acrylamides, such as amine-substituted methacrylates including dimethylaminoethyl methacrylate, tertiary-butylaminoethyl methacrylate and dimethylaminopropyl methacrylamide and the likes; dienes such as 1,3-butadiene and isoprene; vinyl ethers; or combinations thereof. The term "(meth)", i.e., with parentheses, as used herein means that the "meth" is optionally present. For example, "(meth)acrylate" means methacrylate or acrylate.

The first ethylenically unsaturated monomer can also be a functional monomer including for example monomers containing hydroxy, amido, aldehyde, ureido, polyether, glycidylalkyl, keto functional groups or combinations thereof. These functional monomers are generally present in the macromonomer at a level of from 0.1 weight percent to 15 weight percent and more preferably from 0.5 weight percent to 10 weight percent, and most preferably from 1.0 to 3 weight percent, based on the total weight of the graft copolymer. Used herein, all ranges are inclusive and combinable. Examples of functional monomers include ketofunctional monomers such as the acetoacetoxy esters of hydroxyalkyl acrylates and methacrylates (e.g., acetoacetoxyethyl methacrylate) and keto-containing amides (e.g., diacetone acrylamide); allyl alkyl methacrylates or acrylates; glycidylalkyl methacrylates or acrylates; or combinations thereof. Such functional monomers can provide crosslinking if desired.

Typically, the macromonomer also contains as polymerized units less than 10 weight percent, preferably less than 5 weight percent, more preferably less than 2 weight percent and most preferably less than less than 1 weight percent acid containing monomer, based on the total weight of the macromonomer. In a most preferred embodiment, the macromonomer contains no acid containing monomer. Used herein, "acid containing monomer" and "acid functional monomer" are used interchangeably. By "acid containing monomer" it is meant any ethylenically unsaturated monomer that contains one or more acid functional groups or functional groups that are capable of forming an acid (e.g., an anhydride such as methacrylic anhydride or tertiary butyl methacrylate). Examples of acid containing monomers include, for example, carboxylic acid bearing ethylenically unsaturated monomers such as acrylic acid, methacrylic acid, itaconic acid, maleic acid and fumaric acid; acryloxypropionic acid and (meth)acryloxypropionic acid; sulphonic acid-bearing monomers, such as styrene sulfonic acid, sodium vinyl sulfonate, sulfoethyl acrylate, sulfoethyl methacrylate, ethylmethacrylate-2-sulphonic acid, or 2-acrylamido-2-methylpropane sulphonic acid; phosphoethylmethacrylate; the corresponding salts of the acid containing monomer; or combinations thereof.

The macromonomer may contain, as a polymerized unit, a "non-methacrylate monomer". Used herein, a "non-methacrylate monomer" is any first ethylenically unsaturated monomer that is not a methacrylate. For example, butyl acrylate is a first ethylenically unsaturated monomer that is a non-methacrylate monomer. The macromonomer may be free of non-methacrylate monomer, but typically it contains, as polymerized units, at least one non-methacrylate monomer unit, preferably 5 weight percent to 50 weight percent non-methacrylate monomer, more preferably 10 weight percent to 35 weight percent non-methacrylate monomer, and most preferably 15 weight percent to 25 weight percent of non-methacrylate monomer, based on the weight of the macromonomer.

The macromonomer also contains, as polymerized units, less than 1 mole percent, preferably less than 0.5 mole percent, and more preferably no mercapto-olefin compounds, based on the total moles of monomer, present as polymerized units, in the macromonomer. Used herein, "mercapto-olefin" and "mercaptan-olefin" are used interchangeably. These mercapto-olefin compounds are those as disclosed in US-A-5,247,000 by Amick. The mercapto-olefin compounds described in Amick have ester functional groups, which are susceptible to hydrolysis.



In a preferred embodiment of the present invention, the macromonomer is composed of 50 weight percent to 95 weight percent, more preferably from 65 to 90 weight percent, and most preferably from 75 to 85 weight percent, based on total weight of macromonomer, of at least one  $\alpha$ -methyl vinyl monomer, a non  $\alpha$ -methyl vinyl monomer terminated with an  $\alpha$ -methyl vinyl monomer, or combinations thereof. The macromonomer may even be composed of 100 weight percent  $\alpha$ -methyl vinyl monomers, non  $\alpha$ -methyl vinyl monomers terminated with  $\alpha$ -methyl vinyl monomers, or combinations thereof, based on the total weight of the macromonomer. The phrase "non  $\alpha$ -methyl vinyl monomer terminated with an  $\alpha$ -methyl vinyl monomer" means that, when a vinyl monomer bearing no  $\alpha$ -methyl group is present, as polymerized units, in the macromonomer, the macromonomer must be terminated by a unit derived from an  $\alpha$ -methyl vinyl monomer. For example, while styrene might be present, as polymerized units, in a macromonomer chain, that macromonomer chain would be terminated by  $\alpha$ -methyl styrene, or some other  $\alpha$ -methyl vinyl monomer. Suitable  $\alpha$ -methyl vinyl monomers include, for example, methacrylate esters, such as  $C_1$  to  $C_{18}$  normal or branched alkyl esters of methacrylic acid, including methyl methacrylate, ethyl methacrylate, butyl methacrylate, 2-ethylhexyl methacrylate, isobornyl methacrylate, lauryl methacrylate, or stearyl methacrylate; hydroxyalkyl methacrylates such as hydroxyethyl methacrylate; glycidylmethacrylate; phenyl methacrylate; methacrylamide; methacrylonitrile; or combinations thereof.

One skilled in the art will recognize that there are many ways to prepare the macromonomer useful in the present invention. For example, the macromonomer may be prepared by a high temperature (e.g., at least  $150^{\circ}\text{C}$ ) continuous process such as disclosed in US-A-5,710,227 or EP-A-1,010,706, published June 21, 2000. In a preferred continuous process, a reaction mixture of first ethylenically unsaturated monomers is passed through a heated zone having a temperature of at least  $150^{\circ}\text{C}$ , and more preferably at least  $275^{\circ}\text{C}$ . The heated zone may also be maintained at a pressure above atmospheric pressure (e.g., greater than 3,000 kPa = greater than 30 bar). The reaction mixture of monomers may also optionally contain a solvent such as water, acetone, methanol, isopropanol, propionic acid, acetic acid, dimethylformamide, dimethylsulfoxide, methylethylketone, or combinations thereof.

The macromonomer useful in the present invention may also be prepared by polymerizing first ethylenically unsaturated monomers in the presence of a free radical initiator and a catalytic metal chelate chain transfer agent (e.g., a transition metal chelate).

Such a polymerization may be carried out by a solution, bulk, suspension, or emulsion polymerization process. Suitable methods for preparing the macromonomer using a catalytic metal chelate chain transfer agent are disclosed in for example U.S. Patent Nos. 4,526,945, 4,680,354, 4,886,861, 5,028,677, 5,362,826, 5,721,330, and 5,756,605; European  
5 publications EP-A-0199,436, and EP-A-0196783; and PCT publications WO 87/03605, WO 96/15158, and WO 97/34934.

Preferably, the macromonomer useful in the present invention is prepared by an aqueous emulsion free radical polymerization process using a transition metal chelate complex. Preferably, the transition metal chelate complex is a cobalt (II) or (III) chelate  
10 complex such as, for example, dioxime complexes of cobalt (II), cobalt (II) porphyrin complexes, or cobalt (II) chelates of vicinal iminohydroxyimino compounds, dihydroxyimino compounds, diazadihydroxy-iminodialkyldecadienes, or diazadihydroxyiminodialkylundecadienes, or combinations thereof. These complexes may optionally include bridging groups such as  $\text{BF}_2$ , and may also be optionally coordinated with  
15 ligands such as water, alcohols, ketones, and nitrogen bases such as pyridine. Additional suitable transition metal complexes are disclosed in for example U.S. Patent Nos. 4,694,054; 5,770,665; 5,962,609; and 5,602,220. A preferred cobalt chelate complex useful in the present invention is Co II (2,3-dioximinobutane- $\text{BF}_2$ )<sub>2</sub>, the Co III analogue of the aforementioned compound, or combinations thereof. The spatial arrangements of such  
20 complexes are disclosed in for example EP-A-199436 and U.S. Patent No. 5,756,605.

In preparing macromonomer by an aqueous emulsion polymerization process using a transition metal chelate chain transfer agent, at least one first ethylenically unsaturated monomer is polymerized in the presence of a free radical initiator and the transition metal chelate according to conventional aqueous emulsion polymerization techniques. Preferably,  
25 the first ethylenically unsaturated monomer is an  $\alpha$ -methyl vinyl monomer as previously described herein.

The polymerization to form the macromonomer is preferably conducted at a temperature of from 20°C to 150°C, and more preferably from 40°C to 95°C. The solids level at the completion of the polymerization is typically from 5 weight percent to 70 weight  
30 percent, and more preferably from 30 weight percent to 60 weight percent, based on the total weight of the aqueous emulsion.

The concentration of initiator and transition metal chelate chain transfer agent used during the polymerization process is preferably chosen to obtain the desired degree of polymerization of the macromonomer. Preferably, the concentration of initiator is from 0.2 weight percent to 3 weight percent, and more preferably from 0.5 weight percent to 1.5 weight percent, based on the total weight of monomer. Preferably, the concentration of transition metal chelate chain transfer agent is from 5 ppm to 200 ppm, and more preferably from 10 ppm to 100 ppm, based on the total monomers used to form the macromonomer.

The first ethylenically unsaturated monomer, initiator, and transition metal chelate chain transfer agent may be added in any manner known to those skilled in the art to carry out the polymerization. For example, the monomer, initiator and transition metal chelate may all be present in the aqueous emulsion at the start of the polymerization process (i.e., a batch process). Alternatively, one or more of the components may be gradually fed to an aqueous solution (i.e., a continuous or semi-batch process). For example, it may be desired to gradually feed the entire or a portion of the initiator, monomer, and/or transition metal chelate to a solution containing water and surfactant. In a preferred embodiment, at least a portion of the monomer and transition metal chelate are gradually fed during the polymerization, with the remainder of the monomer and transition metal chelate being present in the aqueous emulsion at the start of the polymerization. In this embodiment, the monomer may be fed as is, or suspended or emulsified in an aqueous solution prior to being fed.

Any suitable free radical initiator may be used to prepare the macromonomer. The initiator is preferably selected based on such parameters as its solubility in one or more of the other components (e.g., monomers, water); half life at the desired polymerization temperature (preferably a half life within the range of from about 30 minutes to about 10 hours), and stability in the presence of the transition metal chelate. Suitable initiators include for example azo compounds such as 2,2'-azobis (isobutyronitrile), 4,4'-azobis(4-cyanovaleric acid), 2,2'-azobis [2-methyl-N-(1,1-bis(hydroxymethyl)-2-(hydroxyethyl)]-propionamide, and 2,2'-azobis [2-methyl-N-(2-hydroxyethyl)]-propionamide; peroxides such as t-butyl hydroperoxide, benzoyl peroxide; sodium, potassium, or ammonium persulphate or combinations thereof. Redox initiator systems may also be used, such as for example persulphate or peroxide in combination with a reducing agent such as sodium metabisulphite, sodium bisulfite, sodium formaldehyde sulfoxylate, isoascorbic acid, or combinations thereof.

Metal promoters, such as iron, may also optionally be used in such redox initiator systems. Also, buffers, such as sodium bicarbonate may be used as part of the initiator system.

An emulsifier is also preferably present during the aqueous emulsion polymerization process to prepare the macromonomer. Any emulsifier may be used that is effective in  
5 emulsifying the monomers such as for example anionic, cationic, or nonionic emulsifiers. In a preferred embodiment, the emulsifier is anionic such as for example sodium, potassium, or ammonium salts of dialkylsulphosuccinates; sodium, potassium, or ammonium salts of sulphated oils; sodium, potassium, or ammonium salts of alkyl sulphonic acids, such as sodium dodecyl benzene sulfonate; sodium, potassium, or ammonium salts of alkyl sulphates,  
10 such as sodium lauryl sulfate; ethoxylated alkyl ether sulfates; alkali metal salts of sulphonic acids; C12 to C24 fatty alcohols, ethoxylated fatty acids or fatty amides; sodium, potassium, or ammonium salts of fatty acids, such as Na stearate and Na oleate; or combinations thereof. The amount of emulsifier in the aqueous emulsion is preferably from 0.05 weight percent to 10 weight percent, and more preferably from 0.3 weight percent to 3 weight percent, based on  
15 the total weight of the monomers.

The macromonomer thus prepared is emulsion polymerized with at least one second ethylenically unsaturated monomer to form a copolymer composition containing graft copolymer particles. The polymerization is carried out by providing the macromonomer as water insoluble particles in a macromonomer aqueous emulsion and the second ethylenically  
20 unsaturated monomer in a monomer composition. At least a portion of the macromonomer aqueous emulsion is combined with at least a portion of the monomer composition to form a polymerization reaction mixture that is polymerized in the presence of an initiator.

Although in no way intending to be bound by theory, it is believed that by providing the macromonomer in the form of water insoluble macromonomer particles in an aqueous  
25 emulsion, and the second ethylenically unsaturated monomer in a separate monomer composition, upon combination, the second ethylenically unsaturated monomer diffuses through the aqueous phase and then into the macromonomer particles where the polymerization occurs. Preferably, the diffusion of the second ethylenically unsaturated monomer into the macromonomer particles is evidenced by swelling of the macromonomer  
30 particles. It is an essential feature of the invention that, prior to being combined with the monomer composition, the macromonomers are present in plural discrete particles dispersed in the aqueous phase. Preferably, these plural macromonomer particles have previously been

formed by aqueous emulsion polymerization, and the resultant macromonomer aqueous emulsion is combined with the monomer composition and subsequently polymerized without being isolated. Addition of the monomer composition to the macromonomer aqueous emulsion results initially in the presence of plural monomer droplets in the aqueous emulsion as separate entities distributed among, but not in direct contact with, the plural macromonomer particles. That is, the monomer droplets are separated from the macromonomer particles, and from each other, by an aqueous phase. Individual monomer molecules must then exit the monomer droplet, dissolve in the aqueous phase, diffuse through that aqueous phase to a macromonomer particle, and enter that macromonomer particle where polymerization to form the graft copolymer (preferably, comb copolymer) occurs. Because the water insoluble macromonomers are unable to diffuse through the aqueous phase, it is essential that the monomer droplets not include water insoluble macromonomer if gel formation is to be avoided and if the number of particles initially established by the macromonomer particles is to be maintained during polymerization of monomers with macromonomers.

The macromonomer aqueous emulsion useful in the present invention may be formed in any manner known to those skilled in the art. For example, the macromonomer, produced by any known method, may be isolated as a solid (e.g., spray dried) and emulsified in water. Also, for example, the macromonomer, if prepared via an emulsion or aqueous based polymerization process, may be used as is, or diluted with water or concentrated to a desired solids level.

In a preferred embodiment of the present invention, the macromonomer aqueous emulsion is formed from the emulsion polymerization of at least one first ethylenically unsaturated monomer in the presence of a transition metal chelate chain transfer agent as described previously herein. This embodiment is preferred for numerous reasons. For example, the macromonomer polymerization can be readily controlled to produce a desired particle size distribution (preferably narrow, e.g., polydispersity less than 2). Also, for example, additional processing steps, such as isolating the macromonomer as a solid, can be avoided, leading to better process economics. In addition, the macromonomer, macromonomer aqueous emulsion, and the graft copolymer can be prepared by consecutive steps in a single reactor which is desirable in a commercial manufacturing facility because

process parameters, such as manufacturing cost and particle size distribution, may be optimized.

The "macromonomer aqueous emulsion" useful in the present invention contains from 20 weight percent to 60 weight percent, and more preferably from 30 weight percent to 50 weight percent of at least one water insoluble macromonomer, based on the total weight of macromonomer aqueous emulsion. The macromonomer aqueous emulsion may also contain mixtures of macromonomer. Preferably, the macromonomer aqueous emulsion contains less than 5 weight percent and more preferably less than 1 weight percent of ethylenically unsaturated monomer, based on the total weight of macromonomer aqueous emulsion.

The water insoluble macromonomer particles have a particle size chosen such that, upon addition of monomers, particles of graft copolymer having a desired particle size will be formed. For example, the final graft copolymer particle size is directly proportional to the initial particle size of the macromonomer and the concentration of second ethylenically unsaturated monomer in the polymerization reaction mixture, assuming all the particles participate equally in the polymerization. Preferably, the macromonomer particles have a weight average particle size of from 50 nm to 500 nm, and more preferably from 80 nm to 200 nm as measured by Capillary Hydrodynamic Fractionation technique using a Matec CHDF 2000 particle size analyzer equipped with a HPLC type Ultra-violet detector.

The macromonomer aqueous emulsion may also include one or more emulsifying agents. The type and amount of emulsifying agent is preferably selected in a manner to produce the desired particle size. Suitable emulsifying agents include those previously disclosed for use in preparing the macromonomer by an emulsion polymerization process. Preferred emulsifying agents are anionic surfactants such as, for example, sodium lauryl sulfate, sodium dodecylbenzene sulfonate, sulfated and ethoxylated derivatives of nonylphenols and fatty alcohols. The total level of emulsifying agent, based on the total weight of macromonomer is preferably from 0.2 weight percent to 5 weight percent and more preferably from 0.5 weight percent to 2 weight percent.

The "monomer composition" useful in the present invention contains at least one kind of ethylenically unsaturated monomer. The monomer composition may contain all (i.e., 100%) monomer, or contain monomer dissolved or dispersed in an organic solvent and/or water. Preferably, the level of monomer in the monomer composition is from 50 weight percent to 100 weight percent, more preferably from 60 to 90 weight percent, and most

preferably from 70 to 80 weight percent, based on the total weight of the monomer composition. Examples of organic solvents that may be present in the monomer composition include C<sub>6</sub> to C<sub>14</sub> alkanes. The organic solvent in the monomer composition will be no more than 30 weight percent, and more preferably no more than 5 weight percent, based on the total weight of the monomer composition.

In addition to water and/or organic solvent, the monomer composition may also optionally contain monomers containing functional groups, such as, for example, monomers containing hydroxy, amido, aldehyde, ureido, polyether, glycidylalkyl, keto groups or combinations thereof. These other monomers are generally present in the monomer composition at a level of from 0.5 weight percent to 15 weight percent, and more preferably from 1 weight percent to 3 weight percent based on the total weight of the graft copolymer. Examples of functional monomers include ketofunctional monomers such as the acetoacetoxy esters of hydroxyalkyl acrylates and methacrylates (e.g., acetoacetoxyethyl methacrylate) and keto-containing amides (e.g., diacetone acrylamide); allyl alkyl methacrylates or acrylates; glycidylalkyl methacrylates or acrylates; or combinations thereof. Such functional monomer can provide crosslinking if desired.

In a preferred embodiment, the monomers in the monomer composition are pre-emulsified in water to form a "monomer aqueous emulsion". Preferably, the monomer aqueous emulsion contains monomer droplets having a droplet size from 1 micron to 100 microns, and more preferably from 5 micron to 50 microns. Any suitable emulsifying agent may be used, for example those previously described, to emulsify the monomer to the desired monomer droplet size. Preferably, the level of emulsifying agent, if present, will be from 0.2 weight percent to 2 weight percent based on the total weight of monomer in the monomer composition.

The second ethylenically unsaturated monomer of the monomer composition is preferably selected to provide the desired properties in the resulting comb copolymer composition. Suitable ethylenically unsaturated monomers include for example methacrylate esters, such as C<sub>1</sub> to C<sub>18</sub> normal or branched alkyl esters of methacrylic acid, including methyl methacrylate, ethyl methacrylate, n-butyl methacrylate, 2-ethylhexyl methacrylate, lauryl methacrylate, stearyl methacrylate, isobornyl methacrylate; acrylate esters, such as C<sub>1</sub> to C<sub>18</sub> normal or branched alkyl esters of acrylic acid, including methyl acrylate, ethyl acrylate, n-butyl acrylate and 2-ethylhexyl acrylate; styrene; substituted styrenes, such as methyl styrene,

a-methyl styrene or t-butyl styrene; olefinically unsaturated nitriles, such as acrylonitrile or methacrylonitrile; olefinically unsaturated halides, such as vinyl chloride, vinylidene chloride or vinyl fluoride; vinyl esters of organic acids, such as vinyl acetate; N-vinyl compounds such as N-vinyl pyrrolidone; acrylamide; methacrylamide; substituted acrylamides; substituted methacrylamides; hydroxyalkylmethacrylates such as hydroxyethylmethacrylate; hydroxyalkylacrylates; dienes such as 1,3-butadiene and isoprene; vinyl ethers; or combinations thereof. The ethylenically unsaturated monomer can also be an acid containing monomer or a functional monomer, such as those previously described herein. Preferably, the ethylenically unsaturated monomer of the monomer composition does not contain amino groups.

In a preferred embodiment, the monomer composition includes one or more ethylenically unsaturated monomers selected from C<sub>1</sub> to C<sub>18</sub> normal or branched alkyl esters of acrylic acid, including methyl acrylate, ethyl acrylate, n-butyl acrylate and 2-ethylhexyl acrylate; styrene; substituted styrenes, such as methyl styrene,  $\alpha$ -methyl styrene or t-butyl styrene; butadiene or combinations thereof.

As previously stated, the macromonomer aqueous emulsion and monomer composition are combined to form a "polymerization reaction mixture", and polymerized in the presence of a free radical initiator to form an "aqueous copolymer composition", also referred to herein as an "aqueous dispersion of a comb copolymer". The term "polymerization reaction mixture," as used herein, refers to the resulting mixture formed when at least a portion of the macromonomer aqueous emulsion and at least a portion of the monomer composition are combined. The polymerization reaction mixture may also contain initiator or any other additive used during the polymerization. Thus, the polymerization reaction mixture is a mixture that changes in composition as the macromonomer and monomer in the monomer composition are reacted to form graft copolymer.

The macromonomer aqueous emulsion and monomer composition may be combined in various ways to carry out the polymerization. For example, the macromonomer aqueous emulsion and the monomer composition may be combined prior to the start of the polymerization reaction to form the polymerization reaction mixture. Alternatively, the monomer composition could be gradually fed into the macromonomer aqueous emulsion, or the macromonomer aqueous emulsion could be gradually fed into the monomer composition. It is also possible that only a portion of the macromonomer aqueous emulsion and/or



monomer composition be combined prior to the start of the polymerization with the remaining monomer composition and/or macromonomer aqueous emulsion being fed during the polymerization.

The initiator can also be added in various ways. For example, the initiator may be added in "one shot" to the macromonomer aqueous emulsion, the monomer composition, or a mixture of the macromonomer aqueous emulsion and the monomer composition at the start of the polymerization. Alternatively, all or a portion of the initiator can be co-fed as a separate feed stream, as part of the macromonomer aqueous emulsion, as part of the monomer composition, or any combination of these methods.

The preferred method of combining the macromonomer aqueous emulsion, the monomer composition, and initiator will depend on such factors as the desired graft copolymer composition. For example, the distribution of the macromonomer as a graft along the backbone can be affected by the concentrations of both the macromonomer and the second ethylenically unsaturated monomers at the time of the polymerization. In this regard, a batch process will afford high concentration of both the macromonomer and the second ethylenically unsaturated monomers at the onset of the polymerization whereas a semi-continuous process will keep the second ethylenically unsaturated monomer concentration low during the polymerization. Thus, through the method by which the macromonomer aqueous emulsion and monomer composition are combined, it is possible to control, for example: the number of graft segments, derived from macromonomer, per polymer chain; the distribution of graft segments in each chain, and the length of the polymer backbone.

Initiators useful in polymerizing the macromonomer and second ethylenically unsaturated monomer include any suitable initiator for emulsion polymerizations known to those skilled in the art. The selection of the initiator will depend on such factors as the initiator's solubility in one or more of the reaction components (e.g. monomer, macromonomer, water); and half life at the desired polymerization temperature (preferably a half life within the range of from about 30 minutes to about 10 hours). Suitable initiators include those previously described herein in connection with forming the macromonomer, such as azo compounds such as 4,4'-azobis(4-cyanovaleric acid), peroxides such as t-butyl hydroperoxide; sodium, potassium, or ammonium persulfate; redox initiator systems such as, for example, persulphate or peroxide in combination with a reducing agent such as sodium metabisulfite, sodium bisulfite, sodium formaldehyde sulfoxylate, isoascorbic acid; or

combinations thereof. Metal promoters, such as iron; and buffers, such as sodium bicarbonate, may also be used in combination with the initiator. Additionally, Controlled Free Radical Polymerization (CFRP) methods such as Atom Transfer Radical Polymerization; or Nitroxide Mediated Radical Polymerization may be used. Preferred  
5 initiators include azo compounds such as 4,4'-azobis(4-cyanovaleric acid).

The amount of initiator used will depend on such factors as the copolymer desired and the initiator selected. Preferably, from 0.1 weight percent to 1 weight percent initiator is used, based on the total weight of monomer and macromonomer.

The polymerization temperature will depend on the type of initiator chosen and  
10 desired polymerization rates. Preferably, however, the macromonomer and second ethylenically unsaturated monomer are polymerized at a temperature of from 0°C to 150°C, and more preferably from 20°C to 95°C.

The amount of macromonomer aqueous emulsion and monomer composition added to form the polymerization reaction mixture will depend on such factors as the concentrations of  
15 macromonomer and second ethylenically unsaturated monomer in the macromonomer aqueous emulsion and monomer composition, respectively, and the desired graft copolymer composition. Preferably, the macromonomer aqueous emulsion and monomer composition are added in amounts to provide a graft copolymer containing as polymerized units from 2 weight percent to 90 weight percent, more preferably from 5 weight percent to 50 weight  
20 percent, and most preferably from 5 weight percent to 45 weight percent macromonomer, and from 10 weight percent to 98 weight percent, more preferably from 50 weight percent to 95 weight percent and most preferably from 55 weight percent to 95 weight percent second ethylenically unsaturated monomer.

One skilled in the art will recognize that other components used in conventional  
25 emulsion polymerizations may optionally be used in the method of the present invention. For example, to reduce the molecular weight of the resulting graft copolymer, the polymerization may optionally be conducted in the presence of one or more chain transfer agents, such as n-dodecyl mercaptan, thiophenol; halogen compounds such as bromotrichloromethane; or combinations thereof. Also, additional initiator and/or catalyst may be added to the  
30 polymerization reaction mixture at the completion of the polymerization reaction to reduce any residual monomer, (e.g., chasing agents). Suitable initiators or catalysts include those initiators previously described herein. In addition, the chain transfer capacity of a

macromonomer through addition-fragmentation can be utilized in part to reduce molecular weight through appropriate design of monomer compositions and polymerization conditions. See e.g., E. Rizzardo, *et. al.*, Prog. Pacific Polym. Sci., 1991, 1, 77-88; G. Moad, *et. al.*, WO 96/15157.

5            Preferably, the process of the present invention does not require neutralization of the monomer, or resulting aqueous graft copolymer composition. These components preferably remain in unneutralized form (e.g., no neutralization with a base if acid functional groups are present).

10           The resulting aqueous graft copolymer composition formed by polymerization of the macromonomer and the ethylenically unsaturated monomer in the monomer composition preferably has a solids level of from 30 weight percent to 70 weight percent and more preferably from 40 weight percent to 60 weight percent. The aqueous graft copolymer composition preferably contains graft copolymer particles that are water insoluble and have a particle size of from 60 nm to 500 nm, and more preferably from 80 nm to 200 nm.

15           The graft copolymer (i.e., comb copolymer) formed preferably has a backbone containing, as polymerized units, the second ethylenically unsaturated monomer from the monomer composition, and one or more macromonomer units, as polymerized units, wherein a terminal ethylenically unsaturated group of the macromonomer is incorporated into the backbone and the remainder of the macromonomer becomes a graft segment pendant to the backbone (i.e., a side chain) upon polymerization. Preferably, each side chain is a graft  
20           segment derived from the grafting of one macromonomer to the backbone.

             The degree of polymerization of the graft segments derived from the macromonomer is from 5 to 1,000, preferably from 10 to 1,000, more preferably 10 to 200, and most preferably from 20 to less than 50, where the degree of polymerization is expressed as the  
25           number of polymerized units of ethylenically unsaturated monomer used to form the macromonomer. The weight average molecular weight of the graft copolymer (i.e., of the comb copolymer) is preferably in the range of from 50,000 to 2,000,000, and more preferably from 100,000 to 1,000,000. Weight average molecular weights as used herein can be determined by size exclusion chromatography.

30           The comb copolymer particles of the aqueous copolymer composition can be isolated, for example, by spray drying or coagulation, followed, for example, by forming a coating by powder coating methods, or by redispersing in an aqueous medium. However, it is preferable

to use the aqueous copolymer composition (i.e., the aqueous dispersion of the comb copolymer) as is to form a film. The film may be a free-standing film or a coating on a substrate.

In a preferred embodiment of the present invention, the polymerization is conducted in two stages. In the first stage, the macromonomer is formed in an aqueous emulsion polymerization process, and in the second stage the macromonomer is polymerized with the second ethylenically unsaturated monomer in an emulsion. For efficiency, preferably these two stages are conducted in a single vessel. For example, in the first stage, the macromonomer aqueous emulsion may be formed by polymerizing in an aqueous emulsion at least one first ethylenically unsaturated monomer to form water insoluble macromonomer particles. This first stage polymerization is preferably conducted using a transition metal chelate chain transfer agent as previously described herein. After forming the macromonomer aqueous emulsion, a second emulsion polymerization is preferably performed in the same vessel to polymerize the macromonomer with at least one second ethylenically unsaturated monomer. This second stage may be conducted for example by directly adding (e.g., all at once or by a gradual feed) the monomer composition and initiator to the macromonomer aqueous emulsion. One main advantage of this embodiment is that the macromonomer does not have to be isolated, and the second polymerization can take place simply by adding the monomer composition and initiator to the macromonomer aqueous emulsion. In this preferred embodiment, the particle size and particle size distribution of the plural water insoluble macromonomer particles may be precisely controlled, and later addition of more macromonomer aqueous emulsion would typically not be required, except when, for example, a second mode (particle size and/or composition) of graft copolymer is desired.

In another preferred embodiment of the present invention, the polymerization of the macromonomer and second ethylenically unsaturated monomer is at least partially performed in the presence of an acid containing monomer, acid containing macromonomer, or combinations thereof. The acid containing monomer or acid containing macromonomer may be added in any manner to the polymerization reaction mixture. Preferably, the acid containing monomer or acid containing macromonomer is present in the monomer composition. The acid containing monomer or acid containing macromonomer may also be added as a separate stream to the polymerization reaction mixture.

The amount of acid containing monomer or acid containing macromonomer added to the polymerization reaction mixture is preferably from 0.2 weight percent to 10 weight percent, more preferably from 0.5 weight percent to 5 weight percent, and most preferably from 1 weight percent to 2 weight percent, based on the total weight of monomer and  
5 macromonomer added to the polymerization reaction mixture.

Acid containing monomers which may be used in this embodiment include ethylenically unsaturated monomers bearing acid functional or acid forming groups such as those previously described herein. The "acid containing macromonomer" useful in this embodiment is any low molecular weight polymer having at least one terminal ethylenically  
10 unsaturated group that is capable of being polymerized in a free radical polymerization process, and that is formed from at least one kind of acid containing monomer. Preferably, the amount of acid containing monomer present, as polymerized units, in the acid containing macromonomer is from 50 weight percent to 100 weight percent, more preferably from 90 weight percent to 100 weight percent, and most preferably from 95 weight percent to 100  
15 weight percent.

The acid containing macromonomer may be prepared according to any technique known to those skilled in the art such as those previously described herein. In a preferred embodiment of the present invention, the acid containing macromonomer is prepared by a solution polymerization process using a free radical initiator and transition metal chelate  
20 complex. Such a process is disclosed in, for example, US-A-5,721,330. Preferred acid containing monomers used to form the acid containing macromonomer are  $\alpha$ -methyl vinyl monomers such as methacrylic acid.

In another preferred embodiment of the present invention, a "macromolecular organic compound" having a hydrophobic cavity is present in the polymerization medium used to  
25 form the macromonomer and/or aqueous copolymer composition. Although the macromolecular organic compound may be used to facilitate transport of any ethylenically unsaturated monomer through the aqueous phase of the polymerization reaction mixture, preferably, the macromolecular organic compound is used when copolymerizing ethylenically unsaturated monomers with a water solubility of no greater than 150 millimoles/liter, more  
30 preferably no greater than 50 millimoles/liter. Herein, a water solubility at 25°C to 50°C of no greater than 50 millimoles/liter is referred to as "very low water solubility". Ethylenically unsaturated monomers having very low water solubility include, for example, lauryl

(meth)acrylate and stearyl (meth)acrylate. The macromolecular organic compound may, for example, be added to the monomer composition, the macromonomer aqueous emulsion, or the polymerization reaction mixture used to form the aqueous copolymer composition. Also, for example, the macromolecular organic compound may be added to an aqueous emulsion of ethylenically unsaturated monomer used to form the macromonomer. Suitable techniques for using a macromolecular organic compound having a hydrophobic cavity are disclosed in, for example, US-A-5,521,266.

Preferably, the macromolecular organic compound having a hydrophobic cavity is added to the polymerization reaction mixture to provide a molar ratio of macromolecular organic compound to very low water solubility monomer or macromonomer of from 5:1 to 1:5000 and more preferably from 1:1 to 1:500.

Macromolecular organic compounds having a hydrophobic cavity useful in the present invention include for example cyclodextrin or cyclodextrin derivatives; cyclic oligosaccharides having a hydrophobic cavity such as cyclodextrin, cyclodextrin derivatives, or cyclodextrin derivatives; calixarenes; cavitands; or combinations thereof. Preferably, the macromolecular organic compound is  $\beta$ -cyclodextrin, more preferably methyl- $\beta$ -cyclodextrin.

Monomers having low water solubility include for example primary alkenes; styrene and alkylsubstituted styrene;  $\alpha$ -methyl styrene; vinyltoluene; vinyl esters of  $C_4$  to  $C_{30}$  carboxylic acids, such as vinyl 2-ethylhexanoate, vinyl neodecanoate; vinyl chloride; vinylidene chloride; N-alkyl substituted (meth)acrylamide such as octyl acrylamide and maleic acid amide; vinyl alkyl or aryl ethers with ( $C_3$  - $C_{30}$ ) alkyl groups such as stearyl vinyl ether; ( $C_1$  - $C_{30}$ ) alkyl esters of (meth)acrylic acid, such as methyl methacrylate, ethyl (meth)acrylate, butyl (meth)acrylate, 2-ethylhexyl (meth)acrylate, benzyl (meth)acrylate, lauryl (meth)acrylate, oleyl (meth)acrylate, palmityl (meth)acrylate, stearyl (meth)acrylate; unsaturated vinyl esters of (meth)acrylic acid such as those derived from fatty acids and fatty alcohols; multifunctional monomers such as pentaerythritol triacrylate; monomers derived from cholesterol or combinations thereof.

In another aspect of the present invention an "aqueous copolymer composition" is provided that is preferably produced by the method of the present invention as previously described herein. The aqueous copolymer composition contains a plurality of water insoluble particles of graft copolymer (i.e., comb copolymer particles). The comb copolymer particles

preferably have a weight average particle size of from 50 nm to 1,000 nm, more preferably from 60 nm to 500 nm, and most preferably from 80 nm to 200 nm.

Preferably, the particles of graft copolymer contain from 2 weight percent to 90 weight percent, and more preferably from 5 weight percent to 50 weight percent polymerized units of a macromonomer, based on the total weight of the copolymer, where the  
5 macromonomer preferably has a composition as previously described herein for the water insoluble macromonomer present in the macromonomer aqueous emulsion. The graft copolymer particles also preferably contain from 10 weight percent to 98 weight percent, and more preferably from 50 weight percent to 95 weight percent polymerized units of at least one  
10 second ethylenically unsaturated monomer, based on the total weight of the copolymer. The second ethylenically unsaturated monomer may be any ethylenically unsaturated monomer that provides desirable properties in the copolymer particles, such as those useful in the monomer composition as previously described herein.

Preferably, the backbone of the graft copolymer is linear. Compositionally, the  
15 backbone of the copolymer preferably contains polymerized units of the second ethylenically unsaturated monomer derived from the monomer composition. Preferably, the backbone contains less than 20 mole percent, and more preferably less than 10 mole percent of polymerized macromonomer derived from the macromonomer aqueous emulsion, based on the total moles of monomer, as polymerized units, in the copolymer. Preferably, the Tg of the  
20 backbone of the comb copolymer is from -90°C to 50°C, more preferably -80°C to 25°C, and most preferably -60°C to 0°C. When the comb copolymer is to be used in an aqueous coating composition that will form an elastomeric coating, a caulk, or a sealant, the Tg of the backbone is preferably from -90°C to 25°C, more preferably -80°C to -10°C, and most preferably -60°C to -40°C. The pendant graft segments of the graft copolymer preferably  
25 contain polymerized units of the macromonomer. The carbon atoms of the double bond of the macromonomer, and other atoms such as hydrogen and groups such as methyl directly attached to those carbon atoms, become, as a polymerized unit, part of the backbone of the graft copolymer, while the remainder of the macromonomer becomes a graft segment of the graft copolymer. In a preferred embodiment of the present invention, each graft segment is  
30 derived from one macromonomer. The graft segment contains as polymerized units less than 10 weight percent, preferably less than 5 weight percent, more preferably less than 2 weight percent and most preferably less than 1 weight percent acid containing monomer, based on

the weight of the macromonomer from which it was derived. In a most preferred embodiment, the graft segment contains no acid containing monomer. Further, the graft segment may be free of non-methacrylate monomer, but typically contains, as polymerized units, at least one molecule of non-methacrylate monomer, preferably 5 weight percent to 50 weight percent non-methacrylate monomer, more preferably 10 weight percent to 35 weight percent non-methacrylate monomer, and most preferably 15 weight percent to 25 weight percent of non-methacrylate monomer, based on the weight of the macromonomer from which it was derived. Additionally, the pendant graft segments contain less than 5 weight percent and more preferably less than 1 weight percent of the polymerized second ethylenically unsaturated monomer derived from the monomer composition, based on the total weight of the pendant graft segments.

Preferably, the Tg of the graft segment is from 30°C to 130°C, more preferably from 40°C to 120°C, and most preferably from 50°C to 105°C.

Preferably, the graft segment is present in the comb copolymer at from 1 weight percent to 70 weight percent, more preferably 2 to 45 weight percent, and most preferably 5 to 35 weight percent, based on the weight of the comb copolymer, where the weight of the graft segment is taken as the weight of the macromonomer from which the graft segment was derived.

Preferably, the overall weight average molecular weight of the graft copolymer is from 50,000 to 2,000,000, and more preferably from 100,000 to 1,000,000.

In a preferred embodiment of the present invention, the water insoluble graft copolymer (i.e., comb copolymer) particles further contain from 0.2 weight percent to 10 weight percent, more preferably from 0.5 weight percent to 5 weight percent, and most preferably from 1 weight percent to 2 weight percent of an acid containing macromonomer, based on the total weight of the graft copolymer. The acid containing macromonomer preferably has a composition as previously described herein.

Although in no way intending to be bound by theory, it is believed that the "acid containing macromonomer" is attached to the surface of the water insoluble graft copolymer particles and provides stability. By "attached," as used herein, it is believed that the acid containing macromonomer is bound in some manner (e.g., covalent, hydrogen bonding, ionic) to a polymer chain in the particle. Preferably, the acid containing macromonomer is covalently bound to a polymer chain in the particle. The acid containing macromonomer is



most effective when present at the surface of the graft copolymer particle. As such, it is not necessary that even one acid containing macromonomer unit be incorporated into every graft copolymer. In fact, it is preferable that, when units of acid containing macromonomer are attached to chains of graft copolymer, those chains are at the surface of the graft copolymer particles. It has been found that the acid containing macromonomer provides stability to the particles such that the aqueous copolymer composition produced exhibits unexpected improved shear stability; freeze thaw stability; and stability to additives in formulations, as well as reduction of coagulum during the polymerization. Although improved stability can be achieved using acid containing monomer, these benefits are most dramatic when an acid containing macromonomer is used.

The aqueous copolymer composition in addition to the copolymer particles preferably contains less than 10 weight percent, and more preferably less than 1 weight percent of organic solvent. In a most preferred embodiment, the aqueous copolymer composition contains no organic solvent.

An advantage of using the method of the present invention to prepare the aqueous copolymer composition is that the resulting copolymer composition contains low levels of homopolymer, such as for example homopolymer of second ethylenically unsaturated monomer derived from the monomer composition or homopolymer of macromonomer derived from the macromonomer aqueous emulsion. Preferably the aqueous copolymer composition contains less than 30 weight percent and more preferably less than 20 weight percent of homopolymer of macromonomer, based on the total weight of the graft copolymer. Preferably also the aqueous copolymer composition contains less than 30 weight percent and more preferably less than 20 weight percent of homopolymer of ethylenically unsaturated monomer.

The aqueous coating composition of the present invention may further include a coalescent. The coalescent of the present invention may be any coalescent known to the art. Many common solvents are used in the art as coalescents. It is preferred that the coalescent is present in the amount of from 0 weight percent to 40 weight percent, more preferably 0 weight percent to 20 weight percent, and most preferably 0 weight percent to 5 weight percent, based on the weight of the comb copolymer. In a most preferred embodiment, the aqueous coating composition contains no coalescent.

The aqueous comb copolymer compositions produced by the method of the present invention are useful a aqueous coating compositions in a variety of applications. For example, the aqueous comb copolymer compositions may be used in architectural and industrial coatings including paints, wood coatings, or inks; paper coatings; textile and nonwoven binders and finishes; adhesives; mastics; asphalt additives; floor polishes; leather coatings; plastics; plastic additives; petroleum additives; thermoplastic elastomers or combinations thereof.

When the aqueous comb copolymer composition of the present invention is used as an "aqueous coating composition", it is often desirable to have additional components added to the coating composition to form the final formulation for coating compositions, including clear coatings, primer coatings, semi-gloss paints, glossy paints; caulks, sealants, and traffic paints, described herein. These additional components include, for example, thickeners; rheology modifiers; dyes; sequestering agents; biocides; dispersants; pigments, such as, titanium dioxide, organic pigments, carbon black; extenders, such as calcium carbonate, talc, clays, silicas and silicates; fillers, such as glass or polymeric microspheres, quartz and sand; anti-freeze agents; plasticizers; adhesion promoters such as silanes; coalescents; wetting agents; surfactants; slip additives; crosslinking agents; defoamers; colorants; tackifiers; waxes; preservatives; freeze/thaw protectors; corrosion inhibitors; and anti-flocculants. During application of the aqueous coating composition of the present invention to the surface of a substrate, glass or polymeric microspheres, quartz and sand may be added as part of the that coating composition or as a separate component applied to the surface in a separate step simultaneously with, before, or after the step of application of the aqueous coating composition.

The aqueous coating compositions in which the aqueous copolymer compositions of the present invention are useful include, for example, interior house paints, exterior house paints, automotive paints, appliance paints, inks, and traffic paints.

The amount of pigment and extender in the aqueous coating composition may vary from a pigment volume concentration (PVC) of 0 to 90 and thereby encompass coatings otherwise described in the art, for example, as clear coatings, flat coatings, satin coatings, semi-gloss coatings, gloss coatings, primers, flexible coatings, elastomeric coatings, textured coatings, and automotive coatings. Additionally, systems similar to coatings such as caulks

and sealants can be made with these polymers. The pigment volume concentration is calculated by the following formula:

$$\text{PVC (\%)} = \frac{\text{volume of pigment(s)} + \text{volume extender(s)}}{\text{total dry volume of paint}} \times 100.$$

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The aqueous coating composition of the present invention is prepared by techniques which are well known in the coatings art. First, if the coating composition is to be pigmented, at least one pigment may be well dispersed in an aqueous medium under high shear such as is afforded by a COWLES™ mixer or, in the alternative, at least one predispersed pigment may be used. Then the acrylic emulsion polymer may be added under low shear stirring along with other coatings adjuvants as desired. Alternatively, the emulsion polymer may be present during the pigment dispersion step. The aqueous coating composition may contain conventional coatings adjuvants such as, for example, emulsifiers, buffers, neutralizers, coalescents, thickeners or rheology modifiers, freeze-thaw additives, wet-edge aids, humectants, wetting agents, biocides, antifoaming agents, UV absorbers such as benzophenone, substituted benzophenones, and substituted acetophenones, colorants, waxes, and anti-oxidants. The aqueous coating composition may contain an emulsion polymer not meeting the limitations of the comb copolymer of the present invention, including a film-forming and/or a non-film-forming emulsion polymer. This emulsion polymer may be introduced by blending or in-situ polymerization. When included in the aqueous coating composition, the emulsion polymer not meeting the limitations of the comb copolymer of the present invention is preferably present in an amount of from 1 weight percent to 99 weight percent, more preferably 5 weight percent to 95 weight percent, and most preferably 10 weight percent to 90 weight percent, based on the combined weight of the comb copolymer and the emulsion polymer not meeting the limitations of the comb copolymer of the present invention.

Preferably the aqueous coating composition contains less than 5% VOC by weight based on the total weight of the coating composition; more preferably the aqueous coating composition contains less than 3% VOC by weight based on the total weight of the coating composition; even more preferably the aqueous coating composition contains less than 1.7% VOC by weight based on the total weight of the coating composition. A "volatile organic compound" ("VOC") is defined herein as a carbon containing compound that has a boiling

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point below 280°C at atmospheric pressure, compounds such as water and ammonia being excluded from VOCs.

A "low VOC" coating composition herein is a coating composition which contains less than 5% VOC by weight based on the total weight of the coating composition; preferably  
5 it contains between 1.7% and 0.01% by weight based on the total weight of the coating composition.

Frequently, a VOC is deliberately added to a paint or coating to improve the film properties or to aid in coatings application properties. Examples are glycol ethers, organic esters, aromatic compounds, ethylene and propylene glycol, and aliphatic hydrocarbons. It is  
10 preferred that the coating composition contains less than 5% by weight based on the total weight of the coating composition of the added VOCs and more preferably less than 1.7% by weight based on the total weight of the coating composition of the added VOCs.

Additionally, the low VOC coating composition may contain coalescing agents which are not VOCs. A coalescing agent is a compound that is added to a waterborne emulsion  
15 polymer, paint or coating and which reduces the minimum film forming temperature (MFFT) of the emulsion polymer, paint or coating by at least 1°C. The MFFT is measured using ASTM test method D2354. Examples of a coalescing aid which is not a VOC include a plasticizer, low molecular weight polymer, and surfactants. That is, a non-VOC coalescing agent is a coalescing agent which has a boiling point above 280°C at atmospheric pressure.

20 Typical methods of paint or coating preparation may introduce adventitious VOCs from the emulsion polymer, biocides, defoamers, soaps, dispersants, and thickeners. These typically account for 0.1% VOC by weight based on the total weight of the coating composition. Additional methods such as steam stripping and choice of low VOC containing additives like biocides, defoamers, soaps, dispersants, and thickeners, can be used to further  
25 reduce the paint or coating to less than 0.01% VOC by weight based on the total weight of the coating composition.

In a preferred embodiment the aqueous coating composition has a PVC of 0 to 90 and has less than 5% VOC by weight based on the total weight of the coating composition. In another preferred embodiment The aqueous coating composition has a PVC of greater than  
30 38 and has less than 3% VOC by weight based on the total weight of the coating composition. In an additional embodiment the aqueous coating composition has a PVC of 15

to 85 and has less than 1.6% VOC by weight based on the total weight of the coating composition

The solids content of the aqueous coating composition may be from 5% to 90% by volume. The viscosity of the aqueous polymeric composition may be from 50 KU (Krebs Units) to 140 KU as measured using a Brookfield Digital viscometer KU-1; the viscosities appropriate for different application methods vary considerably, for example caulks and sealants which are beyond the KU range (>100,000 cP).

Conventional coatings application methods such as, for example, brushing, rolling, and spraying methods such as, for example, air-atomized spray, air-assisted spray, airless spray, high volume low pressure spray, and air-assisted airless spray may be used in the method of this invention. Additionally, for some systems other application techniques apply such as, caulk gun, roll coaters, and curtain coaters. The aqueous system may be advantageously applied to substrates such as, for example, plastic, wood, metal, primed surfaces, previously painted surfaces, weathered painted surfaces, glass, composites, and cementitious substrates. Drying is typically allowed to proceed under ambient conditions such as, for example, at 0 °C to 35 °C but may be accelerated with heat or low humidity.

**Experimental Section 1: Preparation of comb copolymers and other copolymers; preparation and testing of aqueous coating compositions containing comb copolymers and other copolymers; and preparation and testing of the coatings formed from the aqueous coating compositions.**

## **Experimental**

### **Molecular Weight Determination using Gel Permeation Chromatography (GPC)**

Gel Permeation Chromatography, otherwise known as size exclusion chromatography, actually separates the members of a distribution of polymer chains according to their hydrodynamic size in solution rather than their molar mass. The system is then calibrated with standards of known molecular weight and composition to correlate elution time with molecular weight. The techniques of GPC are discussed in detail in *Modern Size Exclusion Chromatography*, W. W. Yau, J. J. Kirkland, D. D. Bly; Wiley-Interscience, 1979, and in *A Guide to Materials Characterization and Chemical Analysis*, J. P. Sibilio; VCH, 1988, p.81-84.

For example, the molecular weight information for a low molecular weight sample (e.g., 10,000) may be determined as follows: The sample (an aqueous emulsion containing

low molecular weight particles) is dissolved in THF at a concentration of approximately 0.1% weight sample per volume THF, and shaken for 6 hours, followed by filtration through a 0.45µm PTFE (polytetrafluoroethylene) membrane filter. The analysis is performed by injecting 100µl of the above solution onto 3 columns, connected in sequence and held at 40°C. The three columns are: one each of PL Gel 5 100, PL Gel 5 1,000, and PL Gel 5 10,000, all available from Polymer Labs, Amherst, Massachusetts. The mobile phase used is THF flowing at 1 ml/min. Detection is via differential refractive index. The system was calibrated with narrow polystyrene standards. PMMA-equivalent molecular weights for the sample are calculated via Mark-Houwink correction using  $K=14.1 \times 10^{-3} \text{ ml/g}$  and  $a=0.70$  for the polystyrene standards and  $K=10.4 \times 10^{-3} \text{ ml/g}$  and  $a=0.697$  for the sample

Some embodiments of the invention will now be described in detail in the following Examples. The following abbreviations shown in Table 1 are used in the examples:

**Table 1: Abbreviations**

Abbreviation	Description
A-16-22	Polystep™ A-16-22, anionic surfactant, supplied as 22% solids by Stepan Company, located in Northfield, Illinois.
BA	Butyl acrylate
EA	Ethyl acrylate
MMA	Methyl methacrylate
BMA	Butyl methacrylate
MAA	Methacrylic acid
CoBF	Co(II)-(2,3-dioxyiminobutane-BF <sub>2</sub> ) <sub>2</sub>
CVA	4,4-azobis(4-cyanovaleric acid)
Fe	0.15% Ferrous sulfate in water
GC	Gas chromatograph
SEC	Size exclusion chromatography
HPLC	High performance liquid chromatography
Init.	Initiator
APS	Ammonium persulfate
NaPS	Sodium persulfate
Na <sub>2</sub> CO <sub>3</sub>	Sodium bicarbonate
MM	Macromonomer
PMAA-MM	Poly-methacrylic acid macromonomer
PMMA-MM	Poly-methyl methacrylate macromonomer
Wako VA-044	2,2'-azobis[2-(2-imidazolin-2-yl)propane] dihydrochloride
IR	Infrared spectroscopy

In the Examples, monomer conversion was determined by GC analysis of unreacted monomer using standard methods. Weight percent solids for the macromonomer and copolymers were determined by gravimetric analysis. Particle size of the macromonomer and copolymer compositions were obtained using a Matec CHDF 2000 particle size analyzer equipped with a HPLC type ultra-violet detector.

GPC, Gel Permeation Chromatography, otherwise known as SEC, Size Exclusion Chromatography, separates the members of a distribution of polymer chains according to their hydrodynamic size in solution rather than their molar mass. The system is then calibrated with standards of known molecular weight and composition to correlate elution time with molecular weight. The techniques of GPC are discussed in detail in *Modern Size Exclusion Chromatography*, W. W. Yau, J. J Kirkland, D. D. Bly; Wiley-Interscience, 1979, and in *A Guide to Materials Characterization and Chemical Analysis*, J. P. Sibilis; VCH, 1988, p.81-84.

Macromonomer was measured for number average molecular weight by SEC using a polystyrene standard from Polymer Laboratories (PS-1) having a peak average molecular weight ranging from 580 to 7,500,000 with narrow molecular weight distribution. Conversions from polystyrene to PMMA were made using Mark-Houwink constants. Copolymer compositions were evaluated for number average molecular weight and weight average molecular weight using SEC as follow: the sample is dissolved in THF at a concentration of approximately 0.1% weight sample per volume THF, followed by filtration through a 0.45 $\mu$ m PTFE (polytetrafluoroethylene) membrane filter. The analysis is performed by injecting 100 $\mu$ l of the above solution onto 3 columns connected in sequence and held at 40°C. The three columns are: one each of PL Gel 5 100, PL Gel 5 1,000, and PL Gel 5 10,000, all available from Polymer Labs, Amherst, Massachusetts. The mobile phase used is THF flowing at 1 ml/min. Detection is carried out by the use of ELSD (Evaporative Light Scattering Detector). The system was calibrated with narrow polystyrene standards. PMMA-equivalent molecular weights for the sample are calculated via Mark-Houwink correction using  $K=14.1 \times 10^{-3}$  ml/g and  $\alpha=0.70$  for the polystyrene standards and  $K=10.4 \times 10^{-3}$  ml/g and  $\alpha=0.697$  for the sample.

#### **Examples 1.1 to 1.14. Preparation of Macromonomers by Emulsion Polymerization.**

Macromonomer (MM) was prepared by emulsion polymerization processes in Examples 1.1 to 1.11. The polymerization was conducted in a 5-liter, four-neck round-bottom reaction flask equipped with a mechanical stirrer, temperature control device, condenser, monomer feed line and a nitrogen inlet except for example 1.3 which was prepared in a five-gallon reactor with similar attachments. The specific amounts of water, surfactant, monomers, chain transfer agent (CTA), and initiator used in Examples 1.1 to 1.11 are shown in Table 2. These ingredients were added according to the following procedure: In



a different flask from the reaction flask, a monomer solution was prepared by dissolving the chain transfer agent in the monomer mixture consisting of all the monomers listed in Table 2 under a nitrogen purge. Deionized water and surfactant were introduced into the reaction flask at room temperature to form a water surfactant solution. The water surfactant solution was mixed and heated to 80 °C with stirring under a nitrogen purge. Upon reaching a temperature of 80 °C, and upon complete dissolution of the surfactant, the initiator (CVA) was added to the water surfactant solution with stirring for 2 minutes to permit the initiator to dissolve. After dissolution of the initiator, 63 g of MMA (except for example 1.3, 245 g of MMA) was introduced into the reaction flask and allowed to react for 10 minutes. At the end of 10 minutes, 20 percent by weight of the monomer solution was added to the reaction flask with stirring. Following this initial charge, the remaining monomer solution was fed over a period of 2 hours, with stirring, to form a reaction mixture. At the end of the feed period, the reaction mixture was maintained at 80°C for an additional 2 hours. The reaction mixture was then cooled to room temperature and passed through a filter cloth to remove any coagulum.

Generally, the resulting macromonomer emulsion contained less than 5 weight percent coagulum based on the total weight of macromonomer, and the conversion of monomer was greater than 99 weight percent, based on the total weight of monomer added. The  $M_n$ , weight percent solids and particle size for each macromonomer are reported in Table 2.

**Table 2: Preparation of Macromonomers (MM)**

Ex.	H <sub>2</sub> O (g)	Surf. (g) <sup>(3)</sup>	MMA (g)	EA (g)	BMA (g)	Other (g)	CTA <sup>(1)</sup> (g)	Init. <sup>(2)</sup> (g)	Part. Size (nm)	Mn	Wt % Solids
1.1	2380	55	838	299.4	—	59.8 <sup>(5)</sup>	0.16	12.6	100	9470	33.0
1.2	2380	55	838	299.4	—	59.8 <sup>(5)</sup>	0.16	12.6	100	9180	33.4
1.3	9256	214	4655	—	—	—	0.29	49	84	11210	34.0
1.4	2380	55	838	299.4	—	59.8 <sup>(5)</sup>	0.16	12.6	81	10410	33.4
1.5	2380	55	1160	—	—	—	0.20	12.6	100	3770	32.7
1.6	2300	51	928.8	—	185.8	—	0.08	11.8	99	14050	33.2
1.7	2380	55	580	—	580	—	0.16	3.2	131	9470	33.1
1.8	1190	27.5	508.8	—	—	89.8 <sup>(4)</sup>	0.04	6.3	92	3090	35.5
1.9	2380	55	1197	—	—	—	0.07	12.6	62	8010	33.7
1.10	2380	55	838	299.4	—	59.8 <sup>(5)</sup>	0.16	12.6	100	8960	32.1
1.11	2380	55	838	299.4	—	59.8 <sup>(5)</sup>	0.16	12.6	104	12640	33.3
1.12 <sup>(6)</sup>	2300	51	710	250	—	40 <sup>(5)</sup>	0.16	12.6	90	10000	30
1.13 <sup>(6)</sup>	2300	51	730	250	—	20 <sup>(5)</sup>	0.16	12.6	90	10000	30
1.14 <sup>(6)</sup>	2300	51	750	250	—	—	0.16	12.6	90	10000	30

<sup>(1)</sup> Chain transfer agent (CoBF).<sup>(2)</sup> CVA, supplied by Aldrich as a 75 weight percent aqueous solution of initiator.<sup>(3)</sup> A-16-225 <sup>(4)</sup> Hydroxyethyl methacrylate (HEMA)<sup>(5)</sup> MAA<sup>(6)</sup> The values listed for Examples 1.12-1.14 are the values one would use in preparation of the corresponding macromonomers.**Example 2 Preparation of PMAA-MM By Solution Polymerization.**

MAA macromonomer (PMAA-MM) was prepared by aqueous solution polymerization in a 2-liter baffled flange flask equipped with a mechanical stirrer, condenser, temperature control device, initiator feed lines and a nitrogen inlet. The apparatus was purged with nitrogen for 30 minutes following the addition of 0.018g of CoBF. Deionized water (1080 g) was charged to the flask which was then heated to 55°C under a nitrogen purge. A monomer mixture containing 510 ml of MAA and 0.01 g of CoBF was prepared separately under nitrogen. When the deionized water reached a temperature of 55°C, 1.94 g of initiator (Wako VA-044) was added to the reaction flask. Following the addition of the initiator, the monomer mixture was added over a period of 60 minutes to the reaction flask with stirring. The temperature was then held at 55°C for 2 hours following completion of the monomer mixture feed. Upon cooling the reaction flask to room temperature, the MAA-MM (Example 2.1) was isolated as dried polymer by rotary evaporation. The number average molecular weight ( $M_n$ ) of the MAA-MM was determined by proton nuclear magnetic resonance to be 4030 based on the integration of the vinyl end group with respect to the methyl and methylene groups of the polymer chain.

**Example 3. Preparation of Acrylic graft copolymers by Semi-continuous Process.**

In Examples 3.1 to 3.14, graft copolymers were prepared by a semi-continuous emulsion polymerization process in a 5-liter round bottom flask with four neck equipped with a mechanical stirrer, temperature control device, initiator feed lines and a nitrogen inlet. The specific amounts of Macromonomer (MM, as an emulsion), water, surfactant, monomers, acid containing monomers, and initiator used in Examples 3.1 to 3.14 are shown in Table 3. These ingredients were added according to the following procedure. A monomer emulsion of deionized water (H<sub>2</sub>O #2 in Table 3), surfactant, and monomers (as listed in Table 3) was prepared in a separate flask. Deionized water (H<sub>2</sub>O #1 in Table 3), MM from the example indicated in Table 1 and 20% of the monomer emulsion were introduced into the reaction flask at room temperature to form a reaction mixture. The reaction mixture was heated to 85°C while stirring under a nitrogen purge. Upon reaching 85°C, the initiator and buffer solutions were introduced into the reaction flask. The remaining monomer emulsion was added over a period of 30 minutes with the temperature maintained at 90°C. Upon completion of the feeds, the reaction mixture was maintained at the reaction temperature for a period of 1 hour. The resulting copolymer composition was analyzed for conversion and other properties as described in Table 4. The conversion of BA, determined by standard GC methods, was greater than 99 weight percent, based on the total weight of BA charged. Example 3.15 to 3.17 graft copolymers are prepared by methods identical to those described for the graft copolymers of Examples 3.1 to 3.14.

**Table 3: Preparation of Acrylic Graft Copolymers by Semi-Continuous Emulsion Polymerization**

Example	MM <sup>(1)</sup>		H <sub>2</sub> O #1 (g)	H <sub>2</sub> O #2 (g)	Surf <sup>(2)</sup> (g)	BA (g)	Sty. (g)	MM MAA <sup>(6)</sup>	Init. <sup>(4)</sup> (g)	Buffer <sup>(5)</sup> (g)
	Ex	Amt. (g)								
3.1	1.1	1051	400	500	29.7	895	482	26.3	1.2	1.2
3.2	1.2	1926	50	620	30.8	1168	—	27.6	1.3	1.3
3.3	1.3	1081	525	800	30.8	1443	—	27.4	1.3	1.3
3.4	1.4	919	200	101	14.9	445	111	12.7	0.6	0.6
3.5	1.3	541	500	950	30.8	1627	—	27.6	1.3	1.3
3.6	1.5	592	380	200	28.2	1059	—	25.2	1.2	1.2

3.7	1.6	1915	340	420	30.8	1156	---	27.4	1.3	1.3
3.8	1.7	1457	---	101	14.9	381	---	12.7	0.6	0.6
3.9	1.8	942	110	240	15.8	606	---	14.3	0.6	0.7
3.10	1.2	1051	400	500	29.7	1377	---	26.3	1.2	1.2
3.11	1.9	521	800	600	34.0	1554	---	26.3	1.2	1.2
3.12	1.10	1094	750	300	29.7	1378	---	26.3	1.2	1.2
3.13	1.11	1054	800	250	29.7	1240	138	26.5	1.2	1.2
3.14	1.3	1806	545	203	29.7	1115	---	26.5	1.2	1.2
3.15 <sup>(7)</sup>	1.12	1500	400	200	30	816	---	19.3	1.2	1.2
3.16 <sup>(7)</sup>	1.13	1500	400	200	30	816	---	19.3	1.2	1.2
3.17 <sup>(7)</sup>	1.14	1500	400	200	30	816	---	19.3	1.2	1.2

<sup>(1)</sup> Macromonomer emulsion prepared by method of Example 1.

<sup>(2)</sup> Ethoxylated C<sub>6</sub> to C<sub>18</sub> alkyl ether sulfate having from 1 to 40 ethylene oxide groups per molecule (30% active in water).

<sup>(4)</sup> NaPS dissolved in 10g of water.

5 <sup>(5)</sup> Sodium carbonate dissolved in 15g of water.

<sup>(6)</sup> PMAA-MM (prepared by method of Example 2.1)

<sup>(7)</sup> The values listed for Examples 3.15-3.17 are the values one would use in preparation of the corresponding acrylic graft copolymers (i.e., comb copolymer).

## 10 Characterization of Copolymer Compositions

Graft copolymer compositions prepared in the previous examples were characterized by various analytical techniques to determine wt% solids, particle size, weight average molecular weight, number average molecular weight, and percent incorporation of macromonomer.

15 Determination of the amount of unreacted macromonomer was carried out by HPLC analysis using the following procedure. The copolymer compositions were dissolved in THF and analyzed by gradient elution on an LC-18 column supplied by Supelco, located in Bellefonte, PA such that a well-isolated peak was observed for the unreacted macromonomer. Quantification was carried out by calibrating the detector response using known standards of  
20 the same macromonomer employed in the synthesis. The results of the characterization of Example 3.1 to 3.14 are reported in Table 5 below. The values listed in Table 4 for Examples 3.15 to 3.17 are those one would expect.

**Table 4: Characterization Of Copolymer Compositions**

Example	% Solids	Particle Size (nm)	Mw ( $\times 10^{-3}$ )	Mn ( $\times 10^{-3}$ )	PMMA-MM Incorp. <sup>(1)</sup> (wt%)
3.1	46.4	113	715	196	82
3.2	44.8	59-154 <sup>(2)</sup>	583	158	85
3.3	45.8	119	229	108	91
3.4	44.5	79	367	68	79
3.5	45.6	144	338	22	89
3.6	44.9	150	645	254	99
3.7	44.7	112	632	199	95
3.8	41.7	136	556	301	94
3.9	45.5	118	618	96	87
3.10	46.7	122	238	65	88
3.11	45.9	171	566	141	95
3.12	45.1	135	546	138	86
3.13	42.6	113	515	190	74
3.14	45.5	106	502	96	89
3.15 <sup>(3)</sup>	44	150	500	150	90
3.16 <sup>(3)</sup>	44	150	500	150	90
3.17 <sup>(3)</sup>	44	150	500	150	90

<sup>(1)</sup> Based on the total weight of macromonomer added to reaction vessel.

<sup>(2)</sup> Bimodal distribution

<sup>(3)</sup> The values listed for Examples 3.15-3.17 are the values one would expect in the polymer products.

5

#### **Example 4 Preparation of Blend Polymer Examples**

The blend components were random copolymers prepared by semi-continuous emulsion polymerization in a 5-liter round bottom flask with four neck equipped with a mechanical stirrer, temperature control device, initiator feed lines and a nitrogen inlet. 1,265 g of deionized water and 8.1 g of an ethoxylated C6 to C18 alkyl ether sulfate having from 1 to 40 ethylene oxide groups per molecule (30% active in water) were charged to the reaction flask to generate a reaction mixture. The contents of the flask were heated to 85°C under a nitrogen purge. A monomer emulsion containing deionized water, surfactant, BA, MMA, MAA and a polymerizable ureido monomer, as shown in Table 5, was prepared in a separate flask. Upon reaching 85°C, an initiator solution (7.7 g of APS in 60 g of water) and buffer solution (6 g of Na<sub>2</sub>CO<sub>3</sub> in 60g of water) were introduced into the reaction flask with stirring. The monomer emulsion was fed to the reaction mixture over a period of about 1.5 hours. Upon completion of the feeds, the reaction mixture was maintained at the reaction temperature for 20 minutes. The latex was neutralized to pH = 8 with ammonia. The solids level and particle size were measured to be 47% and 125 nm, respectively. The polymer of Example 4.1 is a soft, film-forming copolymer, while the polymer of Example 4.2, is a hard copolymer that does not form a film.

**Table 5. Preparation of Blend Polymer Examples**

Example	H <sub>2</sub> O	Surfactant <sup>(1)</sup>	BA	MMA	MAA	Other <sup>(2)</sup>
C-4.1	343	68.9	1255	623	29	24
C-4.2	373	65.6	521	1,346	38.6	24

<sup>(1)</sup> Ethoxylated C<sub>6</sub> to C<sub>18</sub> alkyl ether sulfate having from 1 to 40 ethylene oxide groups per molecule (30% active in water).

<sup>(2)</sup> Polymerizable Ureido monomer

### **Examples A, B, and C. Making and Testing of Semigloss Paints**

Semigloss paints were made and tested according to standard practices in the industry and as detailed below.

The Grind was made using ingredients in the ratios in Table A.1, B.1, and C.1 and mixed on a high speed COWLES™ mixer for 20 minutes. The Let Down ingredients were added under low speed mixing in the order given.

**Konig Pendulum Hardness test method.**

Films were dried for 24 hours and 7 days and then tested for film hardness with the Konig pendulum hardness tester, in accordance with ASTM D 4366.

**Abrasive Scrub Resistance test method.**

- 5 A scrub test was run on two specimens of each example following the procedure outlined in ASTM D2486-00 with the following exceptions: a Bird 3 mil film applicator was used to draw down the paints, and the test specimens were held down on each side of the shim midway between the shim and the end of the specimen directly by clamping rather than by means of a gasketed frame as outlined in ASTM D2486-00. Method A of the test method  
10 was otherwise followed.

**Peel block Resistance test method.**

- The peel block resistance test was used for rating the resistance of paint films to blocking, i.e., sticking or fusing when they are placed in contact with each other. ASTM Test Method D4946-99 was followed using the conditions described in their respective results  
15 tables below.

The samples were rated for block resistance on a scale of 0 to 10. Block resistance is reported on a numerical scale of 0 to 10, which corresponds to a subjective tack and seal rating determined by the operator. This rating system is defined in Table 6 in appropriate descriptive terms.

20 **Table 6. Rating Scale for Block Resistance Test.**

Rating	Description	Tack	Seal as percent of contact area
10	perfect	none	None
9	excellent	trace	None
8	very good	slight	None
7	good	slight	None
6	good	moderate	None
5	fair	moderate	None
4	fair	severe	None
3	poor		5-25%
2	poor		25-50%
1	poor		50-75%
0	very poor		100%



**Dirt Pick Up Resistance (DPUR) test method.**

The DPUR test method was used to evaluate gloss/semigloss paints. Coatings were drawn down on a 10.2 cm x 30.5 cm (4 inch x 12 inch) Al panel with a 1.0 mm (40 mil) gap opening bar. The panels were dried in a Constant Temperature and Humidity Room at 23°C (75°F) and 65%RH for a minimum of 7 days. The panels were removed from the room and covered with a dirt slurry for 2 hours minimum until dry, placed in a 60°C oven for 1 hour, allowed to cool, scrubbed with water and cheese cloth to remove the dirt, and allowed to dry at least 2 hours before measuring the initial reflectance on the area without dirt and the dirt scrubbed. The results were reported as the % reflectance retained ( $R_{\text{dirt}}/R_{\text{initial}} \times 100\%$ ).

10 **Table A.1. Adjustment of emulsions to equal weight percent solids (43.5%) and pH (~8.5) to form pre-mixes.**

Ingredient	Comparative Example A.A.p	Comparative Example A.B.p	Exempl e A.1.p	Exempl e A.2.p	Exempl e A.3.p	Exempl e A.4.p <sup>(1)</sup>	Exempl e A.5.p <sup>(1)</sup>	Exempl e A.6.p <sup>(1)</sup>
	<u>Weight</u> (g)	<u>Weight</u> (g)	<u>Weight</u> (g)	<u>Weight</u> (g)	<u>Weight</u> (g)	<u>Weight</u> (g)	<u>Weight</u> (g)	<u>Weight</u> (g)
RHOPLEX™ SG-10M	217.5	-	-	-	-	-	-	-
RHOPLEX™ SF-06	-	233.9	-	-	-	-	-	-
Example 3.1	-	-	234.4	-	-	-	-	-
Example 3.2	-	-	-	242.7	-	-	-	-
Example 3.3	-	-	-	-	237.4	-	-	-
Example 3.15	-	-	-	-	-	247.1	-	-
Example 3.16	-	-	-	-	-	-	247.1	-
Example 3.17	-	-	-	-	-	-	-	247.1
Water	32.5	16.1	14.0	5.7	11.0	1.3	1.3	1.3
Ammonia (28%aqueous)	-	-	1.6	1.6	1.6	1.6	1.6	1.6

<sup>(1)</sup> The values listed for Examples A.4.p through A.6.p are the values one would use in preparation of the corresponding emulsion pre-mixes.

15 The emulsions pre-mixes were made to facilitate the formulation of the coating compositions described in Table A.2.

**Table A.2. Aqueous Gloss/Semigloss Coating Composition**

Ingredient	Comparative Example A.A	Comparative Example A.B	Ex. A.1	Ex. A.2	Ex. A.3	Ex. A.4 <sup>(1)</sup>	Ex. A.5 <sup>(1)</sup>	Ex. A.6 <sup>(1)</sup>
	Weight (g)	Weight (g)	Weight (g)	Weight (g)	Weight (g)	Weight (g)	Weight (g)	Weight (g)
<u>Grind Premix</u>								
TAMOL™ 731A	1.21	1.21	1.21	1.21	1.21	1.21	1.21	1.21
TEGO™ Foamex 810	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10
SURFYNOL™ CT-111	0.20	0.20	0.20	0.20	0.20	0.20	0.20	0.20
TI-PURE™ R- 706	22.84	22.84	22.84	22.84	22.84	22.84	22.84	22.84
Water	0.26	0.26	0.26	0.26	0.26	0.26	0.26	0.26
<u>Let Down</u>								
Propylene Glycol	5.28	5.28	5.28	5.28	5.28	5.28	5.28	5.28
Comparative Example A.A.p	62.65	-	-	-	-	-	-	-
Comparative Example A.B.p	-	62.65	-	-	-	-	-	-
Example A.1.p	-	-	62.65	-	-	-	-	-
Example A.2.p	-	-	-	62.65	-	-	-	-
Example A.3.p	-	-	-	-	62.65	-	-	-
Example A.4.p	-	-	-	-	-	62.65	-	-
Example A.5.p	-	-	-	-	-	-	62.65	-
Example A.6.p	-	-	-	-	-	-	-	62.65
SURFYNOL™ CT-111	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10
ACRYSOL™ RM-2020NPR	1.59	1.59	1.59	1.59	1.59	1.59	1.59	1.59
ACRYSOL™ RM-8W	0.15	0.15	0.15	0.15	0.15	0.15	0.15	0.15
TEXANOL™	2.72	-	-	-	-	-	-	-
DOWANOL™ PPh	-	-	1.36	1.36	1.36	1.36	1.36	1.36

Water	6.63	6.63	6.63	6.63	6.63	6.63	6.63	6.63
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- (1) The values listed for Examples A.4 through A.6 are the values one would use in preparation of the corresponding aqueous gloss/semigloss coating compositions.

**Table A.3. Gloss/Semi-gloss Paint Test Results**

Example Number	Block 23°C 65%RH 60 minutes	Block 49°C 30 minutes	Scrub (cycles)	Gloss (%)	Konig (s)	DPUR (%)	Film Formation 4°C 40%RH
Comparative A.A	9	8	1660	55	27	84	Pass
Comparative A.B	3	0	360	28	18	76	Pass
A.1	7	3	595	53	22	83	Pass
A.2	8	1	300	50	59	81	Pass
A.3	6	2	625	40	18	93	Pass
A.4	8	1	300	50	59	81	Pass
A.5	8	1	275	50	59	81	Pass
A.6	8	1	250	50	59	81	Fail

- (1) The values listed for Examples A.4 through A.6 are the values one would expect in the coatings formed from the corresponding aqueous gloss/semigloss coating compositions.

Examples 3.1 through 3.3 and 3.15 through 3.17 cover a range of macromonomer (i.e., graft segment) and backbone compositions and levels. These do not imply the limits of the invention. The dry coatings of the aqueous gloss/semigloss paint compositions containing these comb copolymers of Examples A.1 through A.3 of this invention provide a set of commercially required properties similar to or superior to that of compositions containing the commercially available emulsion polymers of Comparative Examples A.A and A.B.

**Table B.1. Aqueous Gloss/Semigloss Coating Composition.**

Ingredient	Comparative Example B.A
	Weight (g)
<u>Grind Premix</u>	
TAMOL™ 731A	12.1
TEGO™ Foamex 810	1.0

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SURFYNOL™ CT-111	2.0
TI-PURE™ R-706	228.4
Water	2.6
<u>Let Down</u>	
Example 3.4	612.4
SURFYNOL™ CT-111	1.0
ACRYSOL™ RM-2020NPR	15.9
ACRYSOL™ RM-8W	1.5
DOWANOL™ PPh	13.6
Water	66.3

**Table B.2. Oligomer Premix.**

	Example B.p
Ingredient	Weight (g)
Example 1.4	2.0
Ammonia (7% aqueous solution)	2.0

**Table B.3. Aqueous Gloss/Semigloss Coating Composition.**

5 (post-add of coalescent or oligomer; 5% by weight on polymer solids)

	Example B.1	Example B.2
Ingredient	Weight (g)	Weight (g)
Example B.A	15.00	15.00
DOWANOL™ PPh	0.18	-
Example B.p	-	1.10
Water	1.00	-

**Table B.4. Gloss/Semi-gloss Paint Test Results**

	Block 49°C	Scrub
Example Number	30 minutes	(cycles)

Comparative B.A	4	230
B.1	7	320
B.2	7	312

Examples B.1 and B.2 show the utility of adding oligomer as a means to improve scrub and block resistance as compared to using coalescent agent which, while comparably improving properties, increases VOC (volatile organic content) which is environmentally undesirable. Like amounts of additional coalescent and oligomer give similar property improvements relative to the comparative without the additions. The dry coatings of the aqueous gloss/semigloss paint compositions containing the segmental polymers of Examples B.1 and B.2 of this invention provides a set of commercially required properties similar to or superior to that of composition containing the commercially available emulsion polymer of Comparative Example B.A.

**Table C.1. Adjustment of emulsions to equal weight percent solids (46.5%) and pH (~8.5) to form pre-mixes.**

Ingredient	Comparative C.A.p	Example C.1.p	Example C.2.p	Example C.3.p
	Weight (g)	Weight (g)	Weight (g)	Weight (g)
Example 3.14	-	273.0	409.5	546.0
Example 4.1	508.1	508.1	381.1	254.0
Example 4.2	254.0	-	-	-
Water	37.9	18.9	9.4	-

**Table C.2. Aqueous Gloss/Semigloss Coating Composition**

Ingredient	Comparative Example C.A	Example C.1	Example C.2	Example C.3
	Weight (g)	Weight (g)	Weight (g)	Weight (g)
<u>Grind Premix</u>				
Water	27.47	27.47	27.47	27.47
TAMOL™ 731A	6.59	6.59	6.59	6.59
TEGO™ Foamex 810	0.50	0.50	0.50	0.50
SURFYNOL™ CT-111	1.00	1.00	1.00	1.00

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TI-PURE™ R-706	125.06	125.06	125.06	125.06
KATHON™ LX 1.5%	0.85	0.85	0.85	0.85
<u>Let Down</u>				
Water	7.89	7.89	7.89	7.89
Example C.A.p	264.20	-	-	-
Example C.1.p	-	271.20	-	-
Example C.2.p	-	-	271.20	-
Example C.3.p	-	-	-	271.20
SURFYNOL™ CT-111	0.50	0.50	0.50	0.50
ACRYSOL™ RM-2020NPR	13.20	13.20	13.20	13.20
ACRYSOL™ RM-8W	2.07	2.07	2.07	2.07
Water	74.41	67.41	67.41	67.41

**Table C.3. Gloss/Semi-gloss Paint Test Results**

Example Number	Hard Random Copolymer (Weight %)	Comb Copolymer (Weight %)	Block 49°C 30 minutes	Scrub (cycles)	Gloss (%)	Konig (s)
Comparative C.A	33%	-	1	345	14	20
C.1	-	33%	0	567	27	14
C.2	-	50%	1	458	24	16
C.3	-	67%	5	260	24	21

Examples C.1.p through C.3.p cover a range of comb copolymer levels blended with a soft random copolymer that yield improvements in scrub resistance. The dry coatings of the aqueous gloss/semigloss paint compositions containing the segmental polymers of Examples C.1 through C.3 of this invention provides a set of commercially required properties similar to or superior to that of composition containing the commercially available emulsion polymer of Comparative Example C.A which is a blend of a hard and soft random copolymer as disclosed in US 5,731,377.

#### 10 Example D. Primers

Emulsion blends were used to simulate the performance of Aqueous Primer Compositions.

**Table D.1 Adjustment of emulsions to form clear compositions to be evaluated as Primers**

Ingredient	Example D.A	Example D.B	Example D.1	Example D.2	Example D.3	Example D.4	Example D.5
	Weight (g)	Weight (g)	Weight (g)	Weight (g)	Weight (g)	Weight (g)	Weight (g)
AQUAMAC™ 541	100.0	-	-	-	-	-	-
RHOPLEX™ PR-3232LO	-	100.0	-	-	-	-	-
Example 3.3	-	-	100.0	-	-	-	-
Example 3.5	-	-	-	100.0	-	-	-
Example 3.1	-	-	-	-	100.0	-	-
Example 3.6	-	-	-	-	-	100.0	89.1
Example 1.5	-	-	-	-	-	-	30.6
Ammonium (28%)	-	-	1.0	1.0	1.0	-	1.0
TEXANOL™	1.8	-	-	-	-	1.8	1.8

#### Marker Stain Blocking.

- 5 The marker stain blocking test was used for rating the ability of primer films to block various stains from migrating through the primer and a subsequent topcoat. Marker-stained substrates were prepared by rubbing various markers over a Leneta Form WB chart and allowing them to dry for 1 week prior to use. The markers and suppliers are given in Table 7 below.

10 **Table 7. Description of Markers used in the Marker Stain Blocking Test.**

Type	Marker	Color	Supplier
Solvent-Borne	King Size Permanent Marker	Black	Sanford
Solvent-Borne	King Size Highly Water Resistant	Red	Sanford
Solvent-Borne	Marker Pen	Purple	Paper-Mate
Water-Borne	6000 Large Waterbase Marker	Blue	Eberhard Faber
Water-Borne	Washer Marker	Blue	Crayola
Water-Borne	Marks-A-Lot Washable Markers	Black	Avery Dennison

The test primers were drawn down on the previously stained Leneta Form WB chart with a 0.2 mm (8 mil) gap opening bar and dried at room temperature for 2 hours. A

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commercial high quality interior satin paint (for example, Sherwin-Williams SuperPaint™ Interior Satin Latex) was then applied with a bar wider than the first bar with a 0.38 mm (15 mil) gap opening. The amount of each marker which bled through the topcoat is rated 24 hours after the application of the topcoat. A rating of 5 is no bleed through; a rating of 1 is very severe bleed through. The average of the solvent-borne and water-borne markers are reported as is their sum, the overall marker blocking.

**Table D.2. Primer Test Results**

Example Number	Solvent-Borne Marker Stain Blocking	Water-Borne Marker Stain Blocking	Total Marker Stain Blocking
Comparative D.A	5	5	10
Comparative D.B	5	2	7
D.1	5	4	9
D.2	5	4	9
D.3	5	2	7
D.4	5	5	10
D.5	5	5	10

Examples D.1 through D.5 cover a range of macromonomer (i.e., graft segment) and backbone compositions and levels as well as a blend with oligomer. The dry coatings of the aqueous clear compositions containing the comb polymers of Examples D.1 through D.5 of this invention provides marker stain blocking similar to or superior to that of aqueous clear compositions containing the commercially available emulsion polymers of Comparative Examples D.A and D.B.

## 15 Example E. Clear Coatings

Emulsion blends were used to simulate the performance of Aqueous Clear Coating Compositions.

**Table E.1 Adjustment of emulsions to equal weight percent solids (35%) and pH (~8.5) to form clear compositions to be evaluated as Clear Coatings**

[illegible]



Ingredient	E.A	E.B	E.1	E.2	E.3	E.4	E.5
	Weight (g)	Weight (g)	Weight (g)	Weight (g)	Weight (g)	Weight (g)	Weight (g)
Rhoplex™ JB-101	240.0	-	-	-	-	-	-
RoShield™ 3188	-	220.0	-	-	-	-	-
Example 3.7	-	-	78.30	-	-	-	-
Example 3.8	-	-	-	20.98	-	-	-
Example 3.4	-	-	-	-	39.32	-	-
Example 3.9	-	-	-	-	-	11.45	-
Example 3.5	-	-	-	-	-	-	6.68
Example 1.3	-	-	-	-	-	-	6.74
Water	-	-	21.40	4.02	10.68	3.36	0.58
Ammonium (28%)	-	-	1.36	0.25	0.92	0.22	0.14
DOWANOL™ PPh	-	-	-	0.88	1.75	1.58	-
Butyl Cellosolve (60%)	10.44	29.70	-	-	-	-	-
DOWANOL™ DPM	6.26	-	-	-	-	-	-
DOWANOL™ DPnB	-	4.46	-	-	-	-	-

### Method to Prepare Films

Films were prepared by using the method described in Producing Films of Uniform Thickness of Paint, Varnish, and Related Products on Test Panels, ASTM D 823-95, with the modifications detailed below.

For films applied to aluminum (Panel 3003, supplied by ACT Industries, Inc.; Milwaukee, WI) and polyethylene panels, Practice E was employed (Hand-Held Blade Film Application). For the aluminum panels, the desired dried film thickness was 50.8  $\mu\text{m}$  (2 mils). These films were used for Pendulum Damping Test and Finger Tack Test. For the polyethylene panels, the desired dried film thickness was 101.6  $\mu\text{m}$  (4 mils). These films were used for Tensile Properties Test.

For films applied to White Paper panels (Chart Form WB, supplied by Leneta Company, 15 Whitney Road, Mahwah, NJ), Practice C was employed (Motor-Driven Blade Film Application). The desired dried film thickness was 25.4  $\mu\text{m}$  (1 mil). An auxiliary flattening bar was not used. These films were used for Block Testing.

The gap opening of the blade was chosen using the following approximation:

$$\text{Gap Opening} \approx (\text{Film Thickness} \times 2) \div \% \text{ Solids}$$

Drawdowns were either made in a Constant Temperature and Humidity Room or the panels were placed in the room while still wet. The room conditions were  $23\pm 2^{\circ}\text{C}$  and  $65\pm 5\%$  Relative Humidity. Samples were dried for at least 7 days before testing. If the samples contained coalescent, they were dried for  $3\frac{1}{2}$  days as noted above and then  $3\frac{1}{2}$  days in a vacuum chamber at  $< 0.69\text{ kPa}$  ( $= 0.1\text{ pound/inch}^2$ ) with a small bleed valve open to the atmosphere, providing an air sweep of the chamber. The films were then returned to the Constant Temperature and Humidity Room for at least 3 hours before testing.

#### **Method to Measure Film Thickness**

In order to verify that the blade gap could be used as a good estimate of dry film thickness over all substrates, thickness values for several dry films on aluminum panels were determined using the method described in Measurement of Dry-Film Thickness of Organic Coatings Using Micrometers, ASTM D 1005-95, as detailed in Procedure A, 6.1.5. These measurements agreed to within 15% of those estimated from Equation 1 above. For the films on polyethylene panels used in Tensile Properties Test, the thicknesses of free films were determined using Procedure B.

#### **Preparation of Instron Free Film Samples for the Elongation Test to determine tensile strength.**

The above method was used to prepare free films for testing mechanical properties (tensile strength/elongation, recovery, etc.) on an Instron Tester. This method is applicable to aqueous polymeric dispersions, with or without pigment.

Two strips of masking tape were applied to the films still on the polyethylene sheet across the panel width and 2.54 cm apart. At least three specimens were cut from each test specimen sheet for testing on the Instron Tensile Tester. The thickness of each specimen was determined using a Dial Micrometer, and specimens were selected for Instron Testing if their thickness was uniform to within 10% of the average thickness over the length of the specimen between the areas to be used for gripping by the Instron Tester. Specimens were discarded if they displayed visible flaws, scratches, nicks, tears, or other imperfections likely to cause premature failure during Instron Testing.

#### **Konig Pendulum Hardness**

The Konig Hardness of films were determined using Method for Hardness of Organic Coatings by Pendulum Damping Tests, ASTM D 823-95, with the modifications detailed below.

Dry films were prepared as described above. The Konig Pendulum Hardness, Test Method A, was determined for the films using an oscillation counter as described in Note 1.

#### **Tensile Properties Test**

The Tensile Properties of free films were determined using Method for Tensile Properties of Organic Coatings, ASTM D 2370-98, with the modifications detailed below.

Dry films were prepared on polyethylene panels as described above. After drying, the top surface of the film was treat with the same dry lubricant as used in the film casting. For very tacky films, a light dusting of talc was applied with a camel hair brush. The edges were taped to reinforce the film and it was slowly removed from the panel. If the sample adhered to the panel, it was chilled with ice or dry ice prior to removing. Samples were cut with a scalpel and template to a dimension of 1.27 cm (½") by 7.62 cm (3"). The top and bottom 2.54 cm (1") was reinforced with masking tape leaving a gage length of 2.54 cm (1"). The thickness of these free films was determined as described above.

The samples were tested in a room with the same temperature and relative humidity as that in which they were conditioned. The crosshead speed was 2.54 cm/minute (1"/minute) or 100%/minute for the gage length chosen. The elongation is measured at the point of rupture. The tensile strength is measured at the maximum value. At least 2 samples were tested for each sample. Spurious values were discarded as described in 12.2.2.

#### **Test Method: Finger Tack.**

Tack is the "stickiness" of the surface of a material. It can be qualitatively measured by Finger Tack which is the ability of the material to stick to a clean, dry finger. While subjective is does give a good, reproducible rating of Tack.

Finger Tack is tested by lightly pushing your freshly washed and dried finger on the film on the end of the Aluminum panel and slowly lifting your hand until the panel falls. The position of the panel when it falls yields the rating (Table 8).

**Table 8. Rating system for the Finger Tack Test.**

Position When Panel Falls	Tack Rating	Rating
panel does not lift at all	None	5
up to ~30°	Slight	4

above 30° but before panel lifts off the surface	Moderate	3
panel falls as it lifts from the surface	Very	2
panel is lifted off the surface	Extreme	1

For purposes of reporting the Block Resistance in Table E.2 the ASTM Standard Test Method D 4946-89 was modified to a 1 to 5 scale. Ratings of 0, 1, and 2 are reported as 1; 3 and 4 as 2; 5 and 6 as 3; 7 and 8 as 4; and 9 and 10 as 5.

#### 5 Table E.2. Clear Test Results.

Example	Pendulum Hardness (s)	Tack	Tensile Strength (kPa)	Block	Elongation (%)
E.A	21.0	5	8,163	4	206
E.B	134.4	5	Brittle	4	Brittle
E.1	26.6	5	3,185	4	104
E.2	32.9	4	6,543	4	200
E.3	20.3	5	5,426	4	349
E.4	30.8	5	6,688	4	138
E.5	11.2	4	2,717	1	593

Examples E.1 through E.5 cover a range of macromonomer compositions and levels. The dry films of the aqueous clear compositions containing the comb copolymers of Examples E.1 through E.5 of this invention provide a set of commercially required properties similar to or superior to that of aqueous clear compositions containing the commercially available emulsion polymers of Comparative Examples E.A and E.B.

#### Example F. Elastomeric Coatings

##### Formation of Aqueous Elastomeric Coating Compositions

The Grind was made using ingredients in the ratios in Table F.1 and mixed on a high speed COWLES™ mixer for 20 minutes. The Let Down ingredients were added under low speed mixing in the COWLES™ mixer in the order given.

**Table F.1 Aqueous Elastomeric Coating Composition**

<u>Material</u>	Comparative	
	Example	Example
	F.A	F.1
	Weight	Weight

	(g)	60 (g)
<u>Grind Premix</u>		
Water	152.50	-
Example 3.13	-	317.30
TAMOL™ 850	4.80	4.80
KTTP	1.40	1.40
NOPCO™ NXZ	3.00	3.00
DURAMITE™	422.20	422.20
TI-PURE™ R-960	70.40	70.40
KADOX™ 915	46.90	46.90
<u>Let Down</u>		
RHOPLEX™ EC-1791	470.60	-
Example 3.13	-	302.20
NOPCO™ NXZ	3.00	3.00
TEXANOL™	7.00	-
DOWANOL™ PPh	-	13.2
SKANET™ M-8	2.10	2.10
Ammonia (28%)	1.00	1.00
Propylene Glycol	24.40	24.40
NATROSOL™ 250 MXR	4.20	-

### **Tensile Properties, Permeance, and Low Temperature Flexibility test methods.**

Test for tensile properties, permeance, and low temperature flexibility were done following ASTM D-6083 for acrylic roof coatings with one modification. The low temperature flexibility was measured to obtain the lowest passing temperature on an 1/8" mandrel.

### **Dirt Pick Up Resistance (DPUR) test method.**

The DPUR test method was used to evaluate elastomeric coatings. Coatings were drawn down on a 10.2 cm x 30.5 cm (4 inch x 12 inch) Al panel with a 1.0 mm (40 mil) gap opening bar. The panels were dried in a Constant Temperature and Humidity Room at 23°C (75°F) and 65%RH for a minimum of 4 days. The panels were removed from the room and covered with a dirt slurry for 2 hours minimum until dry, scrubbed with water and cheese cloth to remove the dirt, and allowed to dry at least 2 hours before measuring the initial

reflectance on the area without dirt and the dirt scrubbed. The results were reported as the % reflectance retained ( $R_{\text{dirt}}/R_{\text{initial}} \times 100\%$ ).

#### Alkali Resistance test method.

- Films for alkali resistance testing were prepared as described in ASTM D-6083 (above) for tensile property testing. Test specimens were prepared by cutting films into 7.6 cm x 1.3 cm (3" x 1/2") strips and attaching the strips to individual lids of a 60 ml (2 oz.) glass jar ~ 3/4 filled with 0.5N NaOH. Two sets of samples were set up: one set under room temperature conditions for 3 days and the other in a 60°C (140°F) oven for 3 days. After 3 days the films were qualitatively rated as to how they appeared.

10 **Table F.2 – Elastomeric Coating Results**

<u>Example</u>	DPUR (%)	Low Temperature Flexibility (°C)	Water Permeance (Perms)	Tensile Strength (kPa)	Elongation (%)	Alkali Resistance
Comparative F.A	55.2	-26	56	1903	171	slight swell
F.1	79.8	-26	7	3096	67	no change

- The dry film of the aqueous elastomeric coating composition containing the comb copolymers of Example F.1 of this invention provides a set of commercially required properties similar to or superior to that of composition containing the commercially available emulsion polymer of Comparative Example F.A.

#### Example G. Traffic Paint

##### Formation of Aqueous Traffic Paint Compositions

- The Grind was made using ingredients in Table G.1 and mixed on a high speed COWLES™ mixer for 10 minutes. The Let Down ingredients were added under low speed mixing in the COWLES™ mixer in the order given.

Table G.1 Aqueous Traffic Paint Composition

<u>Material</u>	Comparative	
	Example	Example
	G.A	G.1
	Weight	Weight
	(g)	(g)

62

<u>Grind</u>		
FASTRACK™ 3427	227.7	-
Example 3.1	-	235.0
Water	30.0	-
TAMOL™ 901	2.5	2.7
SURFYNOL™ CT-136	1.4	1.4
DREWPLUS™ L-493	2.7	2.7
TI-PURE™ R-900	50.0	50.0
OMYACARB™ 5	380.3	373.0
<u>Let Down</u>		
Methanol	15.0	15.0
Ammonia (28%)	-	2.1
Polyamine (27%) <sup>(1)</sup>	-	7.0
TEXANOL™	11.5	-
DOWANOL™ PPh	-	5.4
NATROSOL™ 250 HR	6.0	-
(2% solution in water)		
Water	6.4	7.1

(1) The polyamine is disclosed in Patent US 5,804,627

The test paints described in Table G.1 were applied to a 4 inch (10.2 cm) by 12 inch (30.5 cm) aluminum panel using a drawdown blade having a gap of 500  $\mu\text{m}$  (20 mils). After application of the coating, the panels were then allowed to dry at room conditions (23°C and 23% RH) and tested for the following film properties described below and presented in Table G.2.

#### **Early Dirt Pickup Resistance test method.**

Traffic paints were dried for 1 hour, after which an aqueous dispersion of brown iron oxide pigment was applied to a section of the film, allowed to dry for 24 hours, and then washed off with water. The early dirt pickup resistance was assessed by measuring and reporting the L\* whiteness value of this section with a colorimeter.

#### **Early Print Resistance test method.**

Traffic paints were evaluated for early print resistance by the following method. 6.45 cm<sup>2</sup> (1 inch<sup>2</sup>) of cheesecloth was placed on the films after 20 minutes of drying and a #8 rubber stopper and 1 kilogram weight placed on top of the cheesecloth square (to exert 150

g/cm<sup>2</sup> pressure). After 20 minutes, the weight and cheesecloth were removed and the degree of imprint was rated visually (10, no visible imprint; 1, full imprint). This procedure was repeated after the films were dry for 40 minutes.

**Flexibility test method.**

- 5 After the traffic paints dried for 7 days, 1.27 cm (0.5 inch) sections of the panel were bent over a Mandrel tester in accordance with ASTM D522. The films were visually inspected for cracking when bent over the 0.64 and 1.27 cm (0.25 and 0.5 inch) diameter mandrels at room temperature.

**Dry-to-No-Pickup test method.**

- 10 The dry-to-no-pickup time of traffic paints was determined in accordance with ASTM D711 by rolling a traffic paint drying wheel over the wet film. The end point for the dry-to-no-pickup time is defined as the point where no paint adheres to the rubber rings of the test wheel.

**Table G.2 – Traffic Paint Results**

	Comparative Example G.A	Example G.1
Early Print Resistance		
20 minute dry	5	6
40 minute dry	9	10
Pendulum Hardness (s)		
1 day dry	11.2	19.6
7 days dry	33.6	30.8
Early Dirt Pickup (L* value)	68.8	76.7
Flexibility		
¼" mandrel	fail (cracks)	fail (cracks)
½" mandrel	pass	pass
Dry-to-no-pickup (minutes to pass)	3.5	3.0

The dry film of the aqueous traffic paint composition containing the comb copolymer of Example G.1 of this invention provides a set of commercially required properties similar to



or superior to that of composition containing the commercially available emulsion polymer of Comparative Example G.A.

**Table 9. Trademarks and Suppliers**

Trademark	Company	Location
ACRYSOL™	Rohm and Haas Company	Philadelphia, PA, USA
AQUAMAC™	Eastman Chemical Company	Kingsport, TN, USA
DOWANOL™	Dow Chemical	Midland, Michigan, USA
DREWPLUS™	Ashland, Inc.	Covington, KY, USA
DURAMITE™	Fitz Chem Corporation	Elmhurst, IL, USA
FASTRACK™	Rohm and Haas Company	Philadelphia, PA, USA
FOAMEX™	Tego Chemie Service	Essen, Germany
KADOX™	Akrochem Corporation	Akron, OH, USA
KATHON™	Rohm and Haas Company	Philadelphia, PA, USA
NATROSOL™	Hercules, Inc.	Wilmington, DE, USA
NOPCO™	Diamond Shamrock	San Antonio, TX, USA
OMYACARB™	Omya, Inc.	Proctor, VT, USA
RHOPLEX™	Rohm and Haas Company	Philadelphia, PA, USA
ROSHIELD™	Rohm and Haas Company	Philadelphia, PA, USA
SKANE™	Rohm and Haas Company	Philadelphia, PA, USA
SURFYNOL™	Air Products and Chemicals, Inc.	Allentown, PA, USA
TAMOL™	Rohm and Haas Company	Philadelphia, PA, USA
TEGO™	Tego Chemie Service	Essen, Germany
TEXANOL™	Eastman Chemical	Rochester, NY, USA
TI-PURE™	EI DuPont de Nemours, Co.	Wilmington, DE, USA

## 5 Experimental Section 2: Determination of Hard/Soft Balance Advantage Values for Comb Copolymers.

It is a required feature of the present invention that the comb copolymers of the present invention be capable of forming aqueous dispersions having a Hard/Soft Balance Advantage value (i.e., the value of the Hard/Soft Balance Advantage Term) of preferably at least 25%, more preferably from 40% to 1,500%, and most preferably from 100% to 1,000%. The aqueous dispersions used to determine the Hard/Soft Advantage value do not contain all

of the ingredients typically associated with many of the aqueous coating compositions of the present invention exemplified herein. A comb copolymer of the present invention must have the characteristic that an aqueous dispersion of the comb copolymer has a Hard/Soft Balance Advantage value of at least 25%. If a particular comb copolymer is capable of forming aqueous dispersions (prepared as described herein below) having a Hard/Soft Balance Advantage value of at least 25%, that comb copolymer will form aqueous coating compositions of the types described herein above which will themselves have an improved balance of hard and soft properties when compared with a corresponding aqueous coating composition based upon a random copolymer having an identical overall composition.

**10 Examples used in determination of Hard/Soft Advantage Values.**

Some embodiments of the invention will now be described in detail in the following Examples. The following abbreviations shown in Table 1 are used in the examples:

In the Examples, monomer conversion was determined by GC analysis of unreacted monomer using standard methods. Weight percent solids for the macromonomer and copolymers were determined by gravimetric analysis. Particle size of the macromonomer and copolymer compositions were obtained using a Matec CHDF 2000 particle size analyzer  
5 equipped with a HPLC type ultra-violet detector.

GPC, Gel Permeation Chromatography, otherwise known as SEC, Size Exclusion Chromatography, separates the members of a distribution of polymer chains according to their hydrodynamic size in solution rather than their molar mass. The system is then calibrated with standards of known molecular weight and composition to correlate elution time with  
10 molecular weight. The techniques of GPC are discussed in detail in *Modern Size Exclusion Chromatography*, W. W. Yau, J. J Kirkland, D. D. Bly; Wiley-Interscience, 1979, and in *A Guide to Materials Characterization and Chemical Analysis*, J. P. Sibilio; VCH, 1988, p.81-84.

Macromonomer was measured for number average molecular weight by SEC using a  
15 polystyrene standard from Polymer Laboratories (PS-1) having a peak average molecular weight ranging from 580 to 7,500,000 with narrow molecular weight distribution. Conversions from polystyrene to PMMA were made using Mark-Houwink constants. Copolymer compositions were evaluated for number average molecular weight and weight average molecular weight using SEC as follow: the sample is dissolved in THF at a  
20 concentration of approximately 0.1% weight sample per volume THF, followed by filtration through a 0.45 $\mu$ m PTFE (polytetrafluoroethylene) membrane filter. The analysis is performed by injecting 100 $\mu$ l of the above solution onto 3 columns connected in sequence and held at 40°C. The three columns are: one each of PL Gel 5 100, PL Gel 5 1,000, and PL Gel 5 10,000, all available from Polymer Labs, Amherst, Massachusetts. The mobile phase  
25 used is THF flowing at 1 ml/min. Detection is carried out by the use of ELSD (Evaporative Light Scattering Detector). The system was calibrated with narrow polystyrene standards. PMMA-equivalent molecular weights for the sample are calculated via Mark-Houwink correction using  $K=14.1\times 10^{-3}$  ml/g and  $\alpha=0.70$  for the polystyrene standards and  $K=10.4\times 10^{-3}$  ml/g and  $\alpha=0.697$  for the sample.

### 30 Examples 5.1 to 5.9. Preparation of Macromonomers by Emulsion Polymerization

"Macromonomer" ("MM") was prepared by emulsion polymerization processes in Examples 5.1 to 5.6. The polymerization was conducted in a 5-liter, four neck round bottom

reaction flask equipped with a mechanical stirrer, temperature control device, condenser, monomer feed line and a nitrogen inlet except for example 5.1 which was prepared in a 5 gallon reactor with similar attachments. The specific amounts of water, surfactant, monomers, chain transfer agent (CTA), and initiator used in Examples 5.1 to 5.6 are shown in Table 10. These ingredients were added according to the following procedure. In a different flask from the reaction flask, a monomer solution was prepared by dissolving the chain transfer agent in the monomer mixture consisting of all the monomers listed in Table 2 under a nitrogen purge. Deionized water and surfactant were introduced into the reaction flask at room temperature to form a water surfactant solution. The water surfactant solution was mixed and heated to 80 °C with stirring under a nitrogen purge. Upon reaching a temperature of 80 °C, and upon complete dissolution of the surfactant, the initiator (CVA) was added to the water surfactant solution with stirring for 2 minute to permit the initiator to dissolve. After dissolution of the initiator, MMA (245 g for example 5.1 and 63 g for examples 5.2 to 5.6, respectively) was introduced into the reaction flask and allowed to react for 10 minutes. At the end of 10 minutes, 20 percent by weight of the monomer solution was added to the reaction flask with stirring. Following this initial charge, the remaining monomer solution was fed over a period of 2 hours, with stirring, to form a reaction mixture. At the end of the feed period, the reaction mixture was maintained at 80°C for an additional 2 hours. The reaction mixture was then cooled to room temperature and passed through a filter cloth to remove any coagulum.

Generally, the resulting macromonomer emulsion contained less than 5 weight percent coagulum based on the total weight of macromonomer, and the conversion of monomer was over 99 weight percent, based on the total weight of monomer added. The Mn, weight percent solids and particle size for each macromonomer are reported in Table 10.

**Table 10: Preparation of Macromonomers (MM)**

Ex.	H <sub>2</sub> O (g)	Surf. (g) <sup>(3)</sup>	MMA (g)	BMA	EA	MAA	CTA g <sup>(1)</sup>	Init. (g) <sup>(2)</sup>	Part. Size (nm)	Mn	Wt % Solids
5.1	9256	214	4,655	—	—	—	0.29	49	84	11210	34.0
5.2	2380	54.8	838	—	299.4	59.8	0.16	12.6	100	9470	33.0
5.3	2300	51	928.8	185.8	—	—	0.08	11.8	99	14050	33.2
5.4	2380	54.8	838	—	299.4	59.8	0.16	12.6	81	10410	33.4
5.5	2380	55	1,160	—	—	—	0.20	12.6	100	3770	32.7
5.6	2380	55	1,197	—	—	—	0.07	12.6	62	8010	33.7
5.7 <sup>(4)</sup>	2300	51	710	—	250	40	0.16	12.6	90	10000	30
5.8 <sup>(4)</sup>	2300	51	730	—	250	20	0.16	12.6	90	10000	30
5.9 <sup>(4)</sup>	2300	51	750	—	250	—	0.16	12.6	90	10000	30

<sup>(1)</sup> Chain Transfer Agent (CoBF)

<sup>(2)</sup> CVA, supplied by Aldrich as a 75 weight percent aqueous solution of initiator.

<sup>(3)</sup> A-16-22.

5 <sup>(4)</sup> The values listed for Examples 5.7-5.9 are the values one would use in preparation of the corresponding macromonomers.

#### **Example 6. Preparation of PMAA-MM By Solution Polymerization.**

“MAA macromonomer” (“PMAA-MM”) was prepared by aqueous solution polymerization in a 2-liter baffled flange flask equipped with a mechanical stirrer, condenser, temperature control device, initiator feed lines and a nitrogen inlet. The apparatus was purged with nitrogen for 30 minutes after 0.018g of CoBF was added. Deionized water, 1080 g, was charged to the flask and heated to 55°C under a nitrogen purge. A monomer mixture containing 510 ml of MAA and 0.01 g of CoBF was prepared separately under nitrogen. When the deionized water reached a temperature of 55°C, 1.94 g of initiator (Wako VA-044) was added to the reaction flask. Following the addition of the initiator, the monomer mixture was added over a period of 60 minutes to the reaction flask with stirring. The temperature was then held at 55°C for 2 hours following completion of the monomer mixture feed. Upon cooling the reaction flask to room temperature, the MAA-MM (Example 6.1) was isolated as dried polymer by rotary evaporation. The number average molecular weight (Mn) of the MAA-MM was determined by proton nuclear magnetic resonance to be 4030 based on the

integration of the vinyl end group with respect to the methyl and methylene groups of the polymer chain.

**Example 7. Preparation of Acrylic graft copolymers by Semi-continuous Emulsion Polymerization.**

5 In Examples 7.1 to 7.9 and 7.13 to 7.15, graft copolymers were prepared by a semi-continuous emulsion polymerization process in a 5-liter round bottom flask with four neck equipped with a mechanical stirrer, temperature control device, initiator feed lines and a nitrogen inlet. The specific amounts of Macromonomer (MM, as emulsion), water, surfactant, monomers, acid containing monomers, and initiator used in Examples 7.1 to 7.9  
10 and 7.13 to 7.15 are shown in Table 11. These ingredients were added according to the following procedure. A monomer emulsion of deionized water (H<sub>2</sub>O #2 in Table 11), surfactant, and monomers (as listed in Table 11) was prepared in a separate flask. Deionized water (H<sub>2</sub>O #1 in Table 11), MM from the example indicated in Table 10 and 20% of the monomer emulsion were introduced into the reaction flask at room temperature to form a  
15 reaction mixture. The reaction mixture was heated to 85°C while stirring under a nitrogen purge. Upon reaching 85°C, the initiator and buffer solutions were introduced into the reaction flask. The remaining monomer emulsion was added over a period of 30 minutes with the temperature maintained at 90°C. Upon completion of the feeds, the reaction mixture was maintained at the reaction temperature for a period of 1 hours. The resulting copolymer  
20 composition was analyzed for conversion and other properties (Table 13). The conversion of BA and styrene, determined by standard GC methods, was greater than 99 weight percent based on the total weight of monomer charged.

**Table 11: Preparation of Acrylic Graft Copolymers by Semi-Continuous Emulsion Polymerization.**

Ex.	MM <sup>(1)</sup>		H <sub>2</sub> O #1 (g)	H <sub>2</sub> O #2 (g)	Surf. <sup>(2)</sup> (g)	BA (g)	Sty. (g)	Acid (g) <sup>(5)</sup>	Init. <sup>(3)</sup> (g)	Buffer <sup>(4)</sup> (g)
	Ex.	Amt. (g)								
7.1	5.4	919	200	101	14.9	445.4	111	12.7	0.6	0.6
7.2	5.5	892	380	200	28.2	1059	—	25.2	1.2	1.2
7.3	5.5	1783	380	200	28.2	1059	—	25.2	1.2	1.2
7.4	5.1	1806	546	203	29.7	1115	—	26.5	1.2	1.2

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7.5	5.3	1915	340	420	30.8	1156	—	27.4	1.3	1.3
7.6	5.6	521	800	600	34	1554	—	20.5	1.2	1.2
7.7	5.1	2433	100	420	30.8	1011	—	27.4	1.3	1.3
7.8	5.2	1462	400	300	29.7	809.5	436	26.3	1.2	1.2
7.9	5.2	1051	400	500	29.7	895	482	26.3	1.2	1.2
7.10 <sup>(6)</sup> )	5.7	1500	400	200	30	653.5	163	19.2	1.2	1.2
7.11 <sup>(6)</sup> )	5.8	1500	400	200	30	653.5	163	19.2	1.2	1.2
7.12 <sup>(6)</sup> )	5.9	1500	400	200	30	653.5	163	19.2	1.2	1.2
7.13	5.1	541	500	950	30.8	1627	—	27.6	1.3	1.3
7.14	5.1	108	1000	750	30.8	1774	—	27.6	1.3	1.3
7.15	5.1	1081	525	800	30.8	1443	—	27.4	1.3	1.3

<sup>(1)</sup> Macromonomer emulsion prepared by method of Example 5.

<sup>(2)</sup> Ethoxylated C<sub>6</sub> to C<sub>18</sub> alkyl ether sulfate having from 1 to 40 ethylene oxide groups per molecule (30% active in water).

<sup>(3)</sup> NaPS dissolved in 10g of water.

5 <sup>(4)</sup> Sodium carbonate dissolved in 15g of water.

<sup>(5)</sup> PMAA-MM (prepared by method of Example 6.1)

<sup>(6)</sup> The values listed for Examples 7.10-7.12 are the values one would use in preparation of the corresponding acrylic graft copolymers (i.e., comb copolymer).

**Example 8. Preparation of comparative examples.**

In Examples C-4.1 to C-4.6, random copolymers were prepared by semi-continuous emulsion polymerization in a 5-liter round bottom flask with four neck equipped with a mechanical stirrer, temperature control device, initiator feed lines and a nitrogen inlet. The specific amounts of water, surfactant, monomers used in Examples C-4.1 to C-4.6 are shown in Table 12. These ingredients were added according to the following procedure. A monomer emulsion of deionized water (H<sub>2</sub>O #2 in Table 12), surfactant (Surf. #2 in Table 12), and monomers (as listed in Table 12) was prepared in a separate flask. Deionized water (H<sub>2</sub>O #1 in Table 12), and surfactant (Surf. #1, except for C-4.6) were introduced into the reaction flask at room temperature to form a reaction mixture. The reaction mixture was heated to the 85°C while stirring under a nitrogen purge. Upon reaching 85°C, an initiator solution (5.3 g of NaPS except for C-4.6 with 0.54 g, in 30 g of water) and a buffer solution (5.3 g of Na<sub>2</sub>CO<sub>3</sub> except for C-4.6 with 1.21 g, in 30g of water) were introduced into the reaction flask with stirring. The monomer emulsion was fed to the reaction mixture over a period of 3 hours together with an initiator solution (0.8 g NaPS except for C-4.6 with 1.2 g, in 210g of water). Upon completion of the feeds, the reaction mixture was maintained at the reaction temperature for 20 minutes.

**Table 12. Preparation of comparative examples.**

Comp. Ex.	H <sub>2</sub> O #1 (g)	H <sub>2</sub> O #2 (g)	Surf. #1 <sup>(1)</sup> (g)	Surf. #2 <sup>(1)</sup> (g)	EA (g)	BA (g)	MMA (g)	BMA (g)	Sty. (g)	MAA (g)	PMAA-MM <sup>(2)</sup> (g)
C-8.1	400	525	22.3	14.6	130.5	750	361.5	---	187.5	48	22.5
C-8.2	400	525	22.3	14.6	---	852.5	420	105	---	---	22.5
C-8.3	400	675	22.3	14.6	---	795	679.5	---	---	25.5	---
C-8.4	400	525	22.3	14.6	103.5	690	289.5	---	373.5	21	22.5
C-8.5	400	525	22.3	14.6	75	765	210	---	412.5	15	22.5
C-8.6	1395	397	<sup>(3)</sup>	19.4	---	1116.8	615.6	---	---	---	26.3
C-8.7	400	525	22.3	14.6	130.5	750	371.1	---	187.5	38.4	22.5
C-8.8	400	525	22.3	14.6	130.5	750	390.3	---	187.5	19.2	22.5
C-8.9	400	525	22.3	14.6	130.5	750	409.5	---	187.5	---	22.5

<sup>(1)</sup> Ethoxylated C<sub>6</sub> to C<sub>18</sub> alkyl ether sulfate having from 1 to 40 ethylene oxide groups per molecule (30% active in water).

<sup>(2)</sup> PMAA-MM (prepared by method of Example 2.1)

<sup>(3)</sup> 15 g of an acrylic latex seed polymer at 30% solids and particle size of 90 nm was used.



<sup>(6)</sup> The values listed for Examples C-8.7 to C-8.9 are the values one would use in preparation of the corresponding acrylic copolymers.

Graft and Random copolymer compositions prepared in the previous examples were characterized by various analytical techniques to determine wt% solids, particle size, weight average molecular weight, number average molecular weight, and percent incorporation of macromonomer.

Determination of the amount of unreacted macromonomer was carried out by HPLC analysis using the following procedure. The copolymer compositions were dissolved in THF and analyzed by gradient elution on an LC-18 column supplied by Supelco, located in Bellefonte, PA such that a well-isolated peak was observed for the unreacted macromonomer. Quantification was carried out by calibrating the detector response using known standards of the same macromonomer employed in the synthesis. The results of the characterization are reported in Table 13 below.

**Table 13. Characterization Of Copolymer Compositions.**

Ex.	% Solids	Particle Size (nm)	Mw ( $\times 10^{-3}$ )	Mn ( $\times 10^{-3}$ )	PMMA-MM Incorp. <sup>(1)</sup> (wt%)
7.1	44.5	117	366.5	67.7	90
7.2	44.9	150	645	254.4	99
7.3	42.8	132	921.3	145.4	99
7.4	45.5	106	501.7	95.9	87
7.5	44.7	124	631.7	199.2	95
7.6	45.9	171	566	141.4	95
7.7	45.2	105	815.7	132.4	90
7.8	43.9	109	610	147.6	84
7.9	46.4	113	714.7	196.2	82
7.10 <sup>(2)</sup>	44	150	500	150	90
7.11 <sup>(2)</sup>	44	150	500	150	90
7.12 <sup>(2)</sup>	44	150	500	150	90
7.13	45.6	144	337.6	22.1	89

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7.14	45.3	171	340.4	18.7	---
7.15	45.8	119	229	108	91
C-8.1	45.3	96	91.6	3.1	---
C-8.2	37.5	99	146.7	21.7	---
C-8.3	47.3	103	148.0	27.5	---
C-8.4	46.6	93	88.7	3.3	---
C-8.5	45.4	107	299.3	51.9	---
C-8.6	43.7	254	116.8	488.1	---
C-8.7 <sup>(2)</sup>	44	100	150	50	---
C-8.8 <sup>(2)</sup>	44	100	150	50	---
C-8.9 <sup>(2)</sup>	44	100	150	50	---

<sup>(1)</sup> Based on the total weight of macromonomer added to reaction vessel.

<sup>(2)</sup> The values listed for Examples 7.10-7.12 and C-8.7 through C-8.9 are the values one would expect in the polymer products.

#### 5 Example 9. Preparation of a Soft-Hard Elastomeric (SHE) polymer (C-9.1)

The polymer was prepared by a three-stage polymerization process similar to that described in US-A-6060532. The first stage was conducted by semi-continuous emulsion polymerization in a 4-neck 5-liter round-bottom flask equipped with a mechanical stirrer, temperature control device, initiator feed lines and a nitrogen inlet. Deionized water (704 g) was charged to the reaction flask and heated to 92°C. A monomer emulsion containing 366 g of deionized water, 7.4 g of surfactant (A-16-22), 1370 g of BA and 20 g of acrylic acid was prepared in a separate flask. When the deionized water had reached 92°C, an initiator solution (1.77 g of Ammonium Persulfate in 26 g of water) and 67.2 g of a polymer seed (acrylic latex with total solid content of 45% and particle size of 90 nm) were introduced into the reaction flask with stirring. The monomer emulsion was fed to the reaction mixture over a period of about 2 hours, together with a initiator solution containing 1.77 g of APS in 78 g of water. The polymerization temperature was maintain at 85°C. Upon completion of the feeds, the reaction mixture was cooled to 60°C. Aqueous ammonium hydroxide (14% by weight) was added during the cooling followed by 4.1 g of an Fe<sub>2</sub>SO<sub>4</sub> solution (0.2%). At

60°C, 3.8 g of t-butyl hydroperoxide (70%) in 46 g of water and 2.45 g of Sodium sulfoxylate formaldehyde in 46 g of water were added over a period of 45 minutes.

A second monomer emulsion containing 102 g of water, 1.85 g of Polystep™ A-16-22, 359 g of MMA and 8.7 g of MAA was prepared. A solution of Pennstop 2697 (0.89 g supplied by Elf Atochem) in 30 g of water was added to the reaction mixture from stage 1. The monomer emulsion was added to the reaction mixture in one shot followed by 1.55 g of t-butyl hydroperoxide (70%) in 3.7 g of water and 0.65 g of Sodium sulfoxylate formaldehyde in 33 g of water. The reaction mixture was held at the peak exotherm temperature (71-74°C) for 5 minutes, and then cooled to 60°C.

A third monomer emulsion containing 102 g of water, 1.85 g of A-16-22, 359 g of MMA and 8.7 g of MAA was prepared and add to the reaction mixture from stage 2 followed by 1.55 g of t-butyl hydroperoxide (70%) in 3.7 g of water and 0.65 g of Sodium sulfoxylate formaldehyde in 33 g of water. The reaction mixture was held at the peak exotherm temperature (71-74°C) for 5 minutes and cooled to ambient temperature.

The final latex collected after passing through a 100 mesh filter was analyzed to have a solids level of 51.4% and particle size of 430 nm.

**Example 10. Adjustment of Emulsions to similar solids and pH for use in preparing films.**

Portions of the example and comparative emulsions where diluted with deionized water to 35% to 40% weight solids and neutralized with 28% NH<sub>3</sub> to a pH of 8.0 to 8.5. In some examples, oligomer were also adjusted in a similar manner, and coalescing agent where added at the levels described in Table 14. These adjusted emulsions, indicated with an "a" suffix, were allowed to equilibrated at least overnight before further testing.

**Table 14. Composition of the Polymer Portion of Aqueous Dispersion Tested.**

Pol. Ex. No.	Pol. Type (1)	Backbone Composition (2)	Graft Segment Composition (3)	Olig.	% Coa. (4)
7.1a	c/coa	65(78.2 BA/19.5 STY/2.3 g-MAA)	35(70 MMA/25 EA/5 MAA)		5
C-8.1a	r/coa	50 BA/8.7 EA/24.1 MMA/12.5 Sty/3.2 MAA/1.5 g-MAA			5
7.1a	c	65(78.2 BA/19.5 STY/2.3 g-MAA)	35(70 MMA/25 EA/5 MAA)		
C-8.1a	r	50 BA/8.7 EA/24.1 MMA/12.5 Sty/3.2 MAA/1.5 g-MAA			
7.2a	c/o	78.8(97.7 BA/2.3 g-MAA)	21.2(100 MMA) <sup>(7)</sup>	(5)	
C-9.1a	sh	65 (98.6 BA/1.4 AA)/35 (97.6 MMA/2.4 MAA)			
7.3a	c	65(97.7 BA/2.3 g-MAA)	35(100 MMA) <sup>(7)</sup>		

7.4a	c	65(97.7 BA/2.3 g-MAA)	35(100 MMA) <sup>(8)</sup>		
C-8.6a	r	63.5 BA/35 MMA/1.5 MAA			
7.5a	c	63.5 BA/1.5 g-MAA	35(80 MMA/20 BMA)		
C-8.2a	r	63.5 BA/28 MMA/7 BMA/1.5 g-MAA			
7.13a	c/o	88.5 BA/1.5 g-MAA	10(100 MMA)	(6)	
7.7a	c	54.2 BA/1.5 g-MAA	44.3(100 MMA)		
8.3a	r	53 BA/45.3 MMA/1.7 MAA			
7.8a	c	72.5(63.6 BA/34.3 Sty/2.1 g-MAA)	27.5(70 MMA/25 EA/5 MAA)		
C-8.4a	r	46.2 BA/6.9 EA/19.3 MMA/24.9 Sty/1.4 MAA/1.5 MAA			
7.9a	c	80(63.8 BA/34.3 Sty/1.9 g-MAA)	20(70 MMA/25 EA/5 MAA)		
C-8.5a	r	51 BA/5 EA/14 MMA/27.5 Sty/1 MAA/1.5 g-MAA			
7.1a	c	65(78.2 BA/19.5 STY/2.3 g-MAA)	35(70 MMA/25 EA/5 MAA)		
C-8.1a	r	50 BA/8.7 EA/24.1 MMA/12.5 Sty/3.2 MAA/1.5 g-MAA			
7.10a <sup>(9)</sup>	c	65(78.2 BA/19.5 STY/2.3 g-MAA)	35(71 MMA/25 EA/4 MAA)		
C-8.7a <sup>(9)</sup>	r	50 BA/8.7 EA/24.7 MMA/12.5 Sty/2.6 MAA/1.5 g-MAA			
7.11a <sup>(9)</sup>	c	65(78.2 BA/19.5 STY/2.3 g-MAA)	35(73 MMA/25 EA/2 MAA)		
C-8.8a <sup>(9)</sup>	r	50 BA/8.7 EA/26 MMA/12.5 Sty/12.8 MAA/1.5 g-MAA			
7.12a <sup>(9)</sup>	c	65(78.2 BA/19.5 STY/2.3 g-MAA)	35(75 MMA/25 EA)		
C-8.9a <sup>(9)</sup>	r	50 BA/8.7 EA/27.3 MMA/12.5 Sty/1.5 g-MAA			

(1) Used in the tables herein, the following abbreviations have these meanings: "disp." =

"aqueous dispersion"; "ex." = "example"; "no." = "number"; "pol." = "polymer"; "r" =

"random copolymer"; "c" = "comb copolymer"; "sh" = SHE copolymer; "c/coa" = "comb

copolymer" plus "coalescent" at 5 weight %; "r/coa" = "random copolymer" plus

5 "coalescent" at 5 weight %; "c/o" = "comb copolymer / oligomer" blend; "g-MAA" =

"grafted MAA macromonomer"; "olig." = "oligomer"; and "coa." = "coalescent".

(2) When the polymer is a comb copolymer, the numbers inside the parentheses sum to 100.

and represent the weight percent of monomer, present as polymerized units, based on the

weight of the backbone polymer. The number preceding the open parenthesis is the

10 weight percent of backbone polymer, based on the total weight of the comb copolymer.

For random copolymers, the composition of the entire polymer is listed under

"backbone", and no parentheses are required.

(3) When the polymer is a comb copolymer, the numbers inside the parentheses sum to 100

and represent the weight percent of monomer, present as polymerized units, based on the

15 weight of the graft segment. The number preceding the open parenthesis is the weight

percent of graft segment, based on the total weight of the comb copolymer.

- (4) The coalescent, DOWANOL™ PPh (available from Dow Chemical of Midland, Michigan), was added to the aqueous dispersion at 5 weight percent, based on the weight of polymer solids. DOWANOL™ PPh is propyl phenyl glycol ether.
- (5) The oligomer, prepared in Example 1.5, is a macromonomer which is a homopolymer of MMA, having an  $M_n = 3,800$ , and an  $M_w = 5,400$ . The weight ratio of comb copolymer to oligomer is 80:20.
- (6) The oligomer, prepared in Example 1.5, is a macromonomer which is a homopolymer of MMA, having an  $M_n = 3,800$ , and an  $M_w = 5,400$ . The weight ratio of comb copolymer to oligomer is 58:42.
- (7) The graft segment has an  $M_n = 3,800$  and an  $M_w = 5,400$ .
- (8) The graft segment has an  $M_n = 11,200$  and an  $M_w = 16,700$ .
- (9) The values listed for Examples 7.10a through 7.12a and C-8.7a through C-8.9a are the values one would use in preparation of the corresponding acrylic graft copolymers (i.e., comb copolymer).

**Table 15. Glass transition temperatures for the copolymers as calculated using the Fox Equation.**

Pol. Ex. No.	Pol. Type	Tg Backbone (°C)	Tg Graft segment (°C)	Tg Overall (°C)	% Coalescing agent	Tg With Coalescing Agent <sup>(1)</sup> , °C
7.1a	c/coa	-32	65	-5	5	-10
C-8.1a	r/coa			-5	5	-10
7.1a	c	-32	65	-5		
C-8.1a	r			-5		
7.2a	c/o	-51	105	-11		
C-9.1a	sh			-15		
7.3a	c	-51	105	-14		
7.4a	c	-51	105	-14		
C-8.6a	r			-14		
7.5a	c	-51	84	-17		
C-8.2a	r			-17		
7.13a	c/o	-52	105	3		
7.7a	c	-51	105	0		
8.3a	r			1		
7.8a	c	-15	65	4		

C-8.4a	r			3		
7.9a	c	-15	65	-2		
C-8.5a	r			-2		
7.1a	c	-32	65	-5		
C-8.1a	r			-5		
7.10a <sup>(2)</sup>	c	-32	65	-5		
C-8.7a <sup>(2)</sup>	r			-5		
7.11a <sup>(2)</sup>	c	-32	66	-5		
C-8.8a <sup>(2)</sup>	r			-5		
7.12a <sup>(2)</sup>	c	-32	66	-5		
C-8.9a <sup>(2)</sup>	r			-5		

<sup>(1)</sup> Using  $T_g = -75^\circ\text{C}$  for the coalescent.

<sup>(2)</sup> The values listed for Examples 7.10-7.12 and C-8.8 through C-8.10 are the values one would expect in the polymer products.

## 5 Sample preparation methods and test methods for determining Hard/Soft Advantage values.

The methods for forming films on substrates and for forming free-standing films are given in Example E above. Also given in Example E are the test methods for: measuring film thickness; determining König Pendulum Hardness; determining tensile properties, and determining Finger Tack.

The following test methods were also used in determining the Hard/Soft Advantage values.

### Test Method: Peel Block Resistance.

The Peel Block Resistance test was used for rating the resistance of paint films to blocking, i.e., sticking or fusing when they are placed in contact with each other. ASTM Test Method D4946-89 (Reapproved 1999), *Standard Test Method for Blocking Resistance of Architectural Paints*, was followed using a temperature of  $48.9^\circ\text{C}$  ( $120^\circ\text{F}$ ).

The samples were rated for block resistance on a scale of 0 to 10. Block resistance is reported on a numerical scale of 0 to 10, which corresponds to a subjective tack and seal rating determined by the operator. This rating system is defined below in appropriate descriptive terms (Table 16).

**Table 16. Rating Scale for Block Resistance Test.**

Rating	Description	Tack	Seal as percent of contact area
--------	-------------	------	---------------------------------

10	perfect	none	none
9	excellent	trace	none
8	Very good	slight	none
7	Good	slight	none
6	Good	moderate	none
5	Fair	moderate	none
4	Fair	severe	none
3	Poor		5-25%
2	Poor		25-50%
1	Poor		50-75%
0	Very poor		100%

For purposes of calculation of the Block Advantage value,  $A_B$ , the scale of Table 16 and ASTM Standard Test Method D4946-89 was modified to a 1 to 5 scale. Ratings of 0, 1, and 2 are reported as 1; 3 and 4 as 2; 5 and 6 as 3; 7 and 8 as 4; and 9 and 10 as 5.

#### 5 Test Method: Low Temperature Flexibility via Mandrel Bend Test.

The low temperature flexibility of films was determined by using the Mandrel Bend Test of Attached Organic Coatings, ASTM D522-93a, with the modifications detailed below.

Films on Aluminum panels were prepared as previously described. The thickness of several random samples was determined with a dial micrometer gauge. They were  $50.8 \pm 7.6$   $\mu\text{m}$  ( $2 \pm 0.3$  mils), so the target value of  $50.8 \mu\text{m}$  (2 mils) was used in the calculation of % elongation. Test strips were cut from the original panels to a size of 2.54 cm X 10.16 cm (1 inch by 4 inch). These strips and test equipment were conditioned at  $-35^\circ\text{C}$ , or  $-10^\circ\text{C}$ , for 4 hours prior to testing.

Test Method B, the Cylindrical Mandrel Test, was used to determine the elongation of the film. In addition to the specified test equipment, 5.08 cm (2 inch) and 10.16 (4 inch) cm diameter steel tubes were used. The bend time was 1 second instead of the 15 second bend time specified for elongation measurements. No correction was attempted for the difference in bend rate.

The % Elongation and Correction Factors for the 5.08 cm (2 inch) and 10.16 cm (4 inch) diameter mandrels were linearly extrapolated on a log-log plot from those at 2.54 cm

and smaller diameter and are given in Table 17. The calculated Total Elongation for 50.8  $\mu\text{m}$  films is also given.

**Table 17. Elongation, Correction for Film thickness, and Total Elongation**

Mandrel diameter (cm)	Mandrel diameter (inches)	Elongation (%)	Correction for film thickness	Total elongation for 50.8 $\mu\text{m}$ films (%)
0.318	.125	28.00	1.40	30.8
0.635	.250	14.00	0.71	15.4
1.27	.500	6.75	0.38	7.5
2.54	1	3.30	0.21	3.7
5.08	2	1.60	0.11	1.8
10.16	4	0.78	0.06	0.9

5 The test results for the film properties as described above are given in Table 18.

**Table 18. Results for Tests of Hardness and Softness.**

Pol. Ex. No.	Pol. Type	Konig (s)	Tack	Tensile Strength (kPa)	Block <sup>(1)</sup> 48.9°C (120°F) 30 minutes	Elongation at 23°C (%)	Mandrel Elongation At -35°C <sup>(2)</sup> (%)
7.1a	c/coa	21.0	5	5,350	2	410	30.8
C-8.1a	r/coa	4.2	1	2,765	1	664	0.9
7.1a	c	18.9	4	5,343	1	421	3.7
C-8.1a	r	8.4	2	6,267	1	756	1.8
7.2a	c/o	8.4	1	2,710	1	534	30.8
C-9.1a	sh	8.4	2	1,255	1	92	7.5
7.3a	c	poor film	poor film	poor film	poor film	poor film	poor film
7.4a	c	poor film	poor film	poor film	poor film	poor film	poor film
C-8.6a	r	7.0	1	1,634	1	1,119	3.7
7.5a	c	26.6	5	3,185	4	104	30.8
C-8.2a	r	5.6	1	786	1	1,107	7.5
7.13a	c/o	11.2	4	2,717	2	593	30.8
7.7a	c	poor film	poor film	poor film	poor film	poor film	poor film
8.3a	r	17.5	4	4,309	1	387	1.8
7.8a	c	23.8	5	7,619	2	403	1.8
C-8.4a	r	22.4	4	5,936	1	430	0.9



7.9a	c	14.0	4	5,212	1	389	3.7
C-8.5a	r	8.4	2	3,923	1	728	1.8
7.1a	c	18.9	4	5,343	1	421	3.7
C-8.1a	r	8.4	2	6,267	1	756	1.8
7.10a <sup>(3)</sup>	c	18.9	4	5,343	1	421	3.7
C-8.7a <sup>(3)</sup>	r	8.4	2	6,267	1	756	1.8
7.11a <sup>(3)</sup>	c	18.9	4	5,000	1	400	3.7
C-8.8a <sup>(3)</sup>	r	8.4	2	6,267	1	756	1.8
7.12a <sup>(3)</sup>	c	18.9	4	4,500	1	375	3.7
C-8.9a <sup>(3)</sup>	r	8.4	2	6,267	1	756	1.8

(1) The test method for "block resistance" (*supra*) rates block resistance on a scale of 0 to 10 with 0 being "very poor" and 10 being "perfect". For purposes of calculation of the Block Advantage value,  $A_B$ , the scale was modified to a 1 to 5 scale in Table 18. Ratings of 0, 1, and 2 are reported as 1; 3 and 4 as 2; 5 and 6 as 3; 7 and 8 as 4; and 9 and 10 as 5.

5 (2) Dispersion Examples 7.8a and 7.9a and Comparatives C-8.4a and C-8.5a were tested at -10°C to assure that the test temperature was lower than the calculated average Tg of the polymers.

(3) The values listed for Examples 7.10a through 7.12a and C-8.7a through C-8.9a are the values one would expect in the polymer products.

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The calculated Advantage Values for the individual Advantage Terms described above are given in Table 19.

**Table 19. Advantage Values.**

Pol. Ex. No.	Pol. Type	Measures of Hardness				Measures of Softness	
		$A_K$ (%)	$A_T$ (%)	$A_S$ (%)	$A_B$ (%)	$A_E$ (%)	$A_F$ (%)
7.1a	c/coa	400	400	94	100	-38	3322
C-8.1a	r/coa	0	0	0	0	0	0
7.1a	c	125	100	-15	0	-44	106
C-8.1a	r	0	0	0	0	0	0
7.2a	c/o	20	0	66	0	-52	732
C-9.1a	sh	20	100	-23	0	-92	103
7.3a	c	-100	-100	-100	-100	-100	-100
7.4a	c	-100	-100	-100	-100	-100	-100
C-8.6a	r	0	0	0	0	0	0

						81	
7.5a	c	375	400	305	300	-91	311
C-8.2a	r	0	0	0	0	0	0
7.13a	c/o	-36	0	-37	100	53	1611
7.7a	c	-100	-100	-100	-100	-100	-100
8.3a	r	0	0	0	0	0	0
7.8a	c	6	25	28	100	-6	100
C-8.4a	r	0	0	0	0	0	0
7.9a	c	67	100	33	0	-47	106
C-8.5a	r	0	0	0	0	0	0
7.1a	c	125	100	-15	0	-44	106
C-8.1a	r	0	0	0	0	0	0
7.10a <sup>(1)</sup>	c	125	100	-15	0	-44	106
C-8.7a <sup>(1)</sup>	r	0	0	0	0	0	0
7.11a <sup>(1)</sup>	c	125	100	-20	0	-47	106
C-8.8a <sup>(1)</sup>	r	0	0	0	0	0	0
7.12a <sup>(1)</sup>	c	125	100	-28	0	-50	106
C-8.9a <sup>(1)</sup>	r	0	0	0	0	0	0

<sup>(1)</sup> The values listed for Examples 7.10a-7.12a and C-8.7a through C-8.9a are the values one would expect in the polymer products.

The Advantage Values cumulative Hard, Soft and Hard/Soft Balance Advantage

5 Terms as described below are given in Table 20.

**Table 20. Advantage Values: Average Hardness, Softness, and Hard/Soft Balance<sup>(1)</sup>.**

Pol. Ex. No.	Pol. Type	A <sub>Hard</sub> (%)	A <sub>Soft</sub> (%)	A <sub>HSB</sub> (%)
7.1a	c/coa	248	1,642	945
C-8.1a	r/coa	0	0	0
7.1a	c	53	31	42
C-8.1a	r	0	0	0
7.2a	c/o	21	340	181
C-9.1a	sh	24	5	15
7.3a	c	-100	-100	-100
7.4a	c	-100	-100	-100
C-8.6a	r	0	0	0
7.5a	c	345	110	228
C-8.2a	r	0	0	0
7.13a	c/o	7	832	419
7.7a	c	-100	-100	-100
8.3a	r	0	0	0
7.8a	c	40	47	43
C-8.4a	r	0	0	0
7.9a	c	50	29	40
C-8.5a	r	0	0	0
7.1a	c	53	31	42
C-8.1a	r	0	0	0
7.10a <sup>(2)</sup>	c	53	31	42
C-8.7a <sup>(2)</sup>	r	0	0	0
7.11a <sup>(2)</sup>	c	51	29	40
C-8.8a <sup>(2)</sup>	r	0	0	0
7.12a <sup>(2)</sup>	c	49	28	38
C-8.9a <sup>(2)</sup>	r	0	0	0

$$^{(1)} A_{\text{Hard}} = (A_K + A_T + A_S + A_B)/4$$

$$A_{\text{Soft}} = (A_E + A_F)/2$$

$$A_{\text{HSB}} = (A_{\text{Hard}} + A_{\text{Soft}})/2.$$

- 5 The values of the Advantage terms on the right side of each of these equations are listed in Table 20.

<sup>(2)</sup> The values listed for Examples 7.10a through 7.12a and C-8.7a through C-8.9a are the values one would expect in the polymer products.

The values of the Hard/Soft Balance Advantage terms,  $A_{HSB}$ , of Table 20 show that the comb copolymers of the present invention display an improvement in the balance of hardness and softness of at least 25% when compared with random copolymers having the same overall composition. A comparison of a SHE copolymer with a comb copolymer further reveals performance of the comb copolymer which is superior to that of the SHE copolymer (15%) having the same composition.

**Example 11. Adjustment of aqueous dispersions to similar solids and pH for use in preparing films.**

Portions of the example and comparative aqueous dispersions were diluted with deionized water to 35% to 40% weight solids and neutralized with 28%  $\text{NH}_3$  to a pH of 8.0 to 8.5. These adjusted emulsions, as indicated by the "a" suffix, were allowed to equilibrate at least overnight before further blending or testing. Film preparation and testing were done as described above.

**Table 21. Composition of the Polymer Portion of Aqueous Dispersion Tested.**

Pol. Ex. No.	Pol. Type (1)	Backbone Composition (2)	Graft Segment Composition (3)
7.4a	c	65(97.7 BA/2.3 g-MAA)	35(100 MMA)
7.14a	c	98(98.5 BA/1.5 g-MAA)	2(100 MMA)
7.15a	c	80(98.1BA/1.9g-MAA)	20(100 MMA)
7.16a <sup>(4)</sup>	c/c		

(1) Used in the tables herein, the following abbreviations have these meanings: "disp." = "aqueous dispersion" not used????; "ex." = "example"; "no." = "number"; "pol." = "polymer"; "r" = "random copolymer"; "c" = "comb copolymer"; "c/c" = "a blend comprising at least 2 comb copolymers"; "sh" = SHE copolymer; "c/coa" = "comb copolymer" plus "coalescent" at 5 weight %; "r/coa" = "random copolymer" plus "coalescent" at 5 weight %; "c/o" = "comb copolymer / oligomer" blend; "g-MAA" = "grafted MAA macromonomer"; "olig." = "oligomer"; and "coa." = "coalescent".

(2) When the polymer is a comb copolymer, the numbers inside the parentheses sum to 100 and represent the weight percent of monomer, present as polymerized units, based on the weight of the backbone polymer. The number preceding the open parenthesis is the weight percent of backbone polymer, based on the total weight of the comb copolymer.

For random copolymers, the composition of the entire polymer is listed under "backbone", and no parentheses are required.

- (3) When the polymer is a comb copolymer, the numbers inside the parentheses sum to 100 and represent the weight percent of monomer, present as polymerized units, based on the weight of the graft segment. The number preceding the open parenthesis is the weight percent of graft segment, based on the total weight of the comb copolymer.
- (4) Example 7.16a is a blend of 45.5% of Example 7.14a with 55.5% of Example 7.4a yielding an average composition equivalent to Example 7.15a.

10 **Table 22. Results for Tests of Hardness and Softness.**

Pol. Ex. No.	Pol. Type	Konig (s)	Tack	Tensile Strength (kPa)	Block <sup>(1)</sup> 48.9°C (120°F) 30 minutes	Elongation at 23°C (%)	Mandrel Elongation At -35°C (%)
7.4a	c	poor film	poor film	poor film	poor film	poor film	poor film
7.14a	c	9.8	2	579	1	537	30.8
7.15a	c	11.7	4	1,400	2	482	30.8
7.16a	c/c	12.1	4	1,586	1	717	30.8

(1) The test method for "block resistance" (*supra*) rates block resistance on a scale of 0 to 10 with 0 being "very poor" and 10 being "perfect". For purposes of calculation of the Block Advantage value,  $A_B$ , the scale was modified to a 1 to 5 scale in Table 22. Ratings of 0, 1, and 2 are reported as 1; 3 and 4 as 2; 5 and 6 as 3; 7 and 8 as 4; and 9 and 10 as 5.

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The results of film testing are given in Table 22. No Advantage Values are calculated since a common control is not possible over the series of examples as the macromonomer level was changed. Comparisons made by inspection of the data show that blending two comb copolymers which formed a poor film (Example 7.4a) and which had relatively poor performance (Example 7.16a) give a dispersion (Example 7.16a) yielding a film with performance superior to either component used by itself. The blend also has performance better than a dispersion of a comb copolymer having equivalent overall composition (example 7.15a). In these examples, macromonomer level was varied. Similar results are anticipated for varying macromonomer, oligomer, and backbone composition and level,  $T_g$ , hydrophilicity, and molecular weight as well as particle size of the individual comb

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copolymers or oligomer dispersions. One or more of the blend components could be a polymer other than a comb-copolymer.

We claim:

1. An aqueous coating composition comprising a plurality of comb copolymer particles:  
5 wherein said comb copolymer particles comprise a comb copolymer;  
wherein said comb copolymer comprises a backbone and at least one graft segment  
attached thereto; and  
wherein said comb copolymer is characterized in that an aqueous dispersion comprising  
said comb copolymer has a Hard/Soft Balance Advantage value of at least 25%.
- 10 2. The aqueous coating composition of claim 1, wherein said comb copolymer has a  
weight average molecular weight of 50,000 to 2,000,000.
3. The aqueous coating composition of claim 1:  
wherein said graft segment is derived, as a polymerized unit, from a macromonomer;  
and  
15 wherein said graft segment comprises, as polymerized units, less than 5 weight percent  
acid containing monomer, based on the total weight of said macromonomer.
4. The aqueous coating composition of claim 1:  
wherein said graft segment is derived, as a polymerized unit, from a macromonomer;  
and  
20 wherein said graft segment comprises, as polymerized units, less than 1 weight percent  
acid containing monomer, based on the total weight of said macromonomer.
5. The aqueous coating composition of claim 1, wherein said graft segment comprises, as  
polymerized units, at least one unit derived from a non-methacrylate monomer.
6. The aqueous coating composition of claim 1:  
25 wherein said graft segment is derived, as a polymerized unit, from a macromonomer;  
and  
wherein said graft segment comprises, as polymerized units, from 5 weight percent to  
50 weight percent of a non-methacrylate monomer, based on the weight of said  
macromonomer.
- 30 7. The aqueous coating composition of claim 1:  
wherein said graft segment is derived, as a polymerized unit, from a macromonomer;  
and

wherein said graft segment has a degree of polymerization of from 10 to 1,000, where the degree of polymerization of said graft segment is expressed as the degree of polymerization of said macromonomer.

8. The aqueous coating composition of claim 1:

5 wherein said graft segment is derived, as a polymerized unit, from a macromonomer;  
and

wherein said graft segment has a degree of polymerization of from 10 to less than 50, where the degree of polymerization of said graft segment is expressed as the degree of polymerization of said macromonomer.

10 9. The aqueous coating composition of claim 1, wherein said graft segment has a glass transition temperature of 30 to 130 °C.

10. The aqueous coating composition of claim 1, wherein said backbone has a glass transition temperature of -90°C to 50°C.

11. The aqueous coating composition of claim 1, wherein said graft segment is present in  
15 the amount of 1 to 70 weight percent based on the weight of said comb copolymer.

12. The aqueous coating composition of claim 1, further comprising a coalescent in an amount of from 0 weight percent to 40 weight percent, based on the weight of said comb copolymer.

13. The aqueous coating composition of claim 1, further comprising an oligomer in an  
20 amount of 1 to 50 weight percent, based on the weight of said comb copolymer.

14. The aqueous coating composition of claim 1, wherein said comb copolymer is produced by a polymerization method comprising the steps of:

(a) forming a macromonomer aqueous emulsion comprising a plurality of water-insoluble particles of macromonomer, wherein said macromonomer comprises  
25 polymerized units of at least one first ethylenically unsaturated monomer, said macromonomer further having:

(i) a degree of polymerization of from 10 to 1000;

(ii) at least one terminal ethylenically unsaturated group;

(iii) less than 5 weight percent polymerized acid-containing monomer, based on  
30 the weight of said macromonomer; and

(iv) less than one mole percent of polymerized mercaptan-olefin compounds;



- (b) forming a monomer composition comprising at least one second ethylenically unsaturated monomer; and
  - (c) combining at least a portion of said macromonomer aqueous emulsion and at least a portion of said monomer composition to form a polymerization reaction mixture; and
  - (d) polymerizing said macromonomer with said second ethylenically unsaturated monomer in the presence of an initiator to produce said plurality of comb copolymer particles.
15. The aqueous coating composition of claim 14, wherein said polymerization reaction mixture further comprises a macromolecular organic compound.
16. An method of forming a dry coating comprising the steps of:
- (a) forming an aqueous coating composition comprising a plurality of comb copolymer particles:
    - wherein said comb copolymer particles comprise a comb copolymer;
    - wherein said comb copolymer comprises a backbone and at least one graft segment attached thereto; and
    - wherein said comb copolymer is characterized in that an aqueous dispersion comprising said comb copolymer has a Hard/Soft Balance Advantage value of at least 25%;
  - (b) applying said coating composition to a substrate; and
  - (c) drying, or allowing to dry, said applied coating composition.
17. The method of claim 16, wherein said comb copolymer is produced by a polymerization method comprising the steps of:
- (a) forming a macromonomer aqueous emulsion comprising a plurality of water-insoluble particles of macromonomer, wherein said macromonomer comprises polymerized units of at least one first ethylenically unsaturated monomer, said macromonomer further having:
    - (i) a degree of polymerization of from 10 to 1000;
    - (ii) at least one terminal ethylenically unsaturated group;
    - (iii) less than 5 weight percent polymerized acid-containing monomer, based on said macromonomer; and
    - (iv) less than one mole percent of polymerized mercaptan-olefin compounds;

- 5 (b) forming a monomer composition comprising at least one second ethylenically unsaturated monomer;
- (c) combining at least a portion of said macromonomer aqueous emulsion and at least a portion of said monomer composition to form a polymerization reaction mixture; and
- (d) polymerizing said macromonomer with said second ethylenically unsaturated monomer in the presence of an initiator to produce said plurality of comb copolymer particles.
- 10 18. The method of claim 17, wherein said polymerization reaction mixture further comprises a macromolecular organic compound.
19. A dry coating comprising a comb copolymer:  
wherein said comb copolymer comprises a backbone and at least one graft segment attached thereto; and  
wherein said comb copolymer is characterized in that an aqueous dispersion comprising  
15 said comb copolymer has a Hard/Soft Balance Advantage value of at least 25%.
20. A dry coating produced by the method of claim 16.

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(54) Title: **AQUEOUS DISPERSIONS OF COMB COPOLYMERS AND COATINGS PRODUCED THEREFROM**

(57) Abstract: An aqueous coating composition comprising a comb copolymer is disclosed. A method of forming a coating from the aqueous coating composition, and a coating formed by that method are also disclosed, as is a method of forming the comb copolymer. The comb copolymer is characterized in that aqueous dispersions of the comb copolymer have a Hard/Soft Balance Advantage value of at least 25 %. The aqueous coating composition is capable of producing coatings having an excellent balance of hard and soft properties.



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Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the International search (name of data base and, where practical, search terms used)

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Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
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